

Some
Fundamentals of Cryogenic
and Module Engineering
with regard to SRF Technology

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Overview

- First part: Some theory
- Second part: More practical aspects
(cryomodule design considerations)

Too much items..... and still incomplete.....

But let's see how far we can proceed.....

My sources:

- LINDEKRYOTECHNIK AG Switzerland, H.Herzog
- AERZEN Compressors Germany
- AIR LIQUIDE France
- WEKA Valves Switzerland
- VDI-Seminars Germany
- AD-Pressure-Vessel-Code
- ASME Code
- My colleagues from INFN, FNAL, Cornell-University, J-LAB, KEK, BESSY, DESY and Steve van Sciver
- others

First part: tutorial objectives

after this part, we should remember:

- The meaning of ,***cryogenic***'
- Carnot refrigerator efficiency
- ,***COP***' of a refrigerator
- Some Helium refrigerator cycles
- Some ,quantum properties' of matter at low temperatures
- Some useful Helium II properties
- Some typical cooling cycles
- Some fundamentals of thermal insulation

Cryogenic Fundamentals

Why is ,Cryogenic' separated from ,usual' cooling engineering ?

Use of ,conventional' superconductors like Nb requires cooling
at liquid helium temperatures

Due to basic thermodynamic laws, the efficiency of refrigerators is quite low at these temperatures (,Carnot cycle') – the cooling is very expensive !

-> excellent thermal insulation is required

-> refrigerators should work very efficient to come closer to the Carnot cycle

-> we have to deal with ,quantum properties' of matter at these temperatures:
decrease of specific heat, heat transfer, superconductivity, superfluidity.....

-> helium is the only coolant (low heat of vaporization, leak tightness, purification techniques.....)

-> careful engineering is needed: choice of materials, welding procedures, quality control, pressure vessel code requirements.....

Definition: ,CRYOGENIC‘

Traditional (you can find in textbooks) : $T < 120 \text{ K}$

[My personal view: $T < 77 \text{ K}$ (LN2 cooling is no ,real‘ cryogenic)]

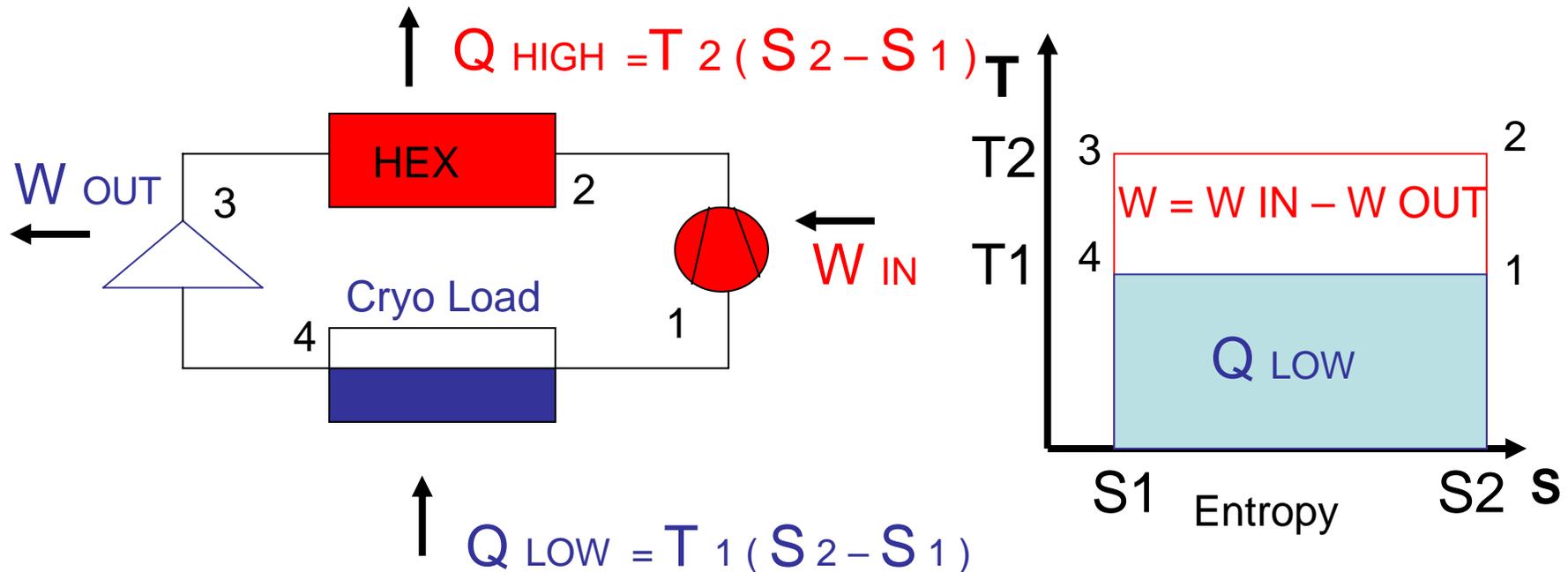
Physicist view : temperatures where characteristic quantum states of matter dominate ($C_p \rightarrow 0$, Helium II, conventional superconductivity.....)

HERE: The engineering, which is required to specify, design, construct and operate cooling systems and cryostats for superconducting RF cavities at liquid Helium temperatures.

Basic laws of thermodynamics

1. Energy conservation
2. Entropy can never decrease spontaneously in a closed system: $0 \leq \Delta S$ - corresponds to
,The Carnot Cycle is the most efficient cycle that exist‘
3. $S \rightarrow 0$ for $T \rightarrow 0$ for an ideal crystal
corresponds to $C_p \rightarrow 0$
(Engineers forget zero-point energy)

Carnot Refrigeration Cycle

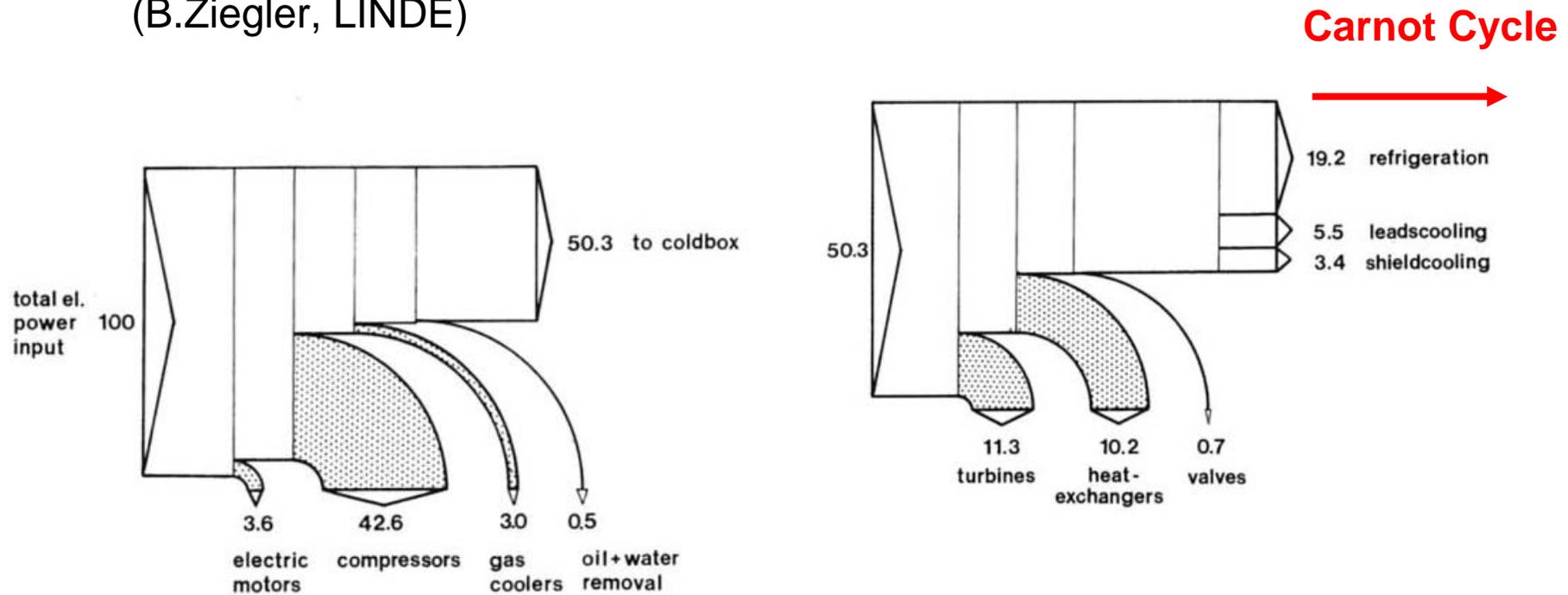


$$\eta_{Carnot} = \frac{\text{Useful Refrigeration}}{\text{Work Input}} = \frac{Q_{LOW}}{Q_{HIGH} - Q_{LOW}} = \frac{T_1}{T_2 - T_1}$$

COP = Coefficient of Performance = $1/\eta_{Carnot}$

Sources of Irreversibility

(B.Ziegler, LINDE)



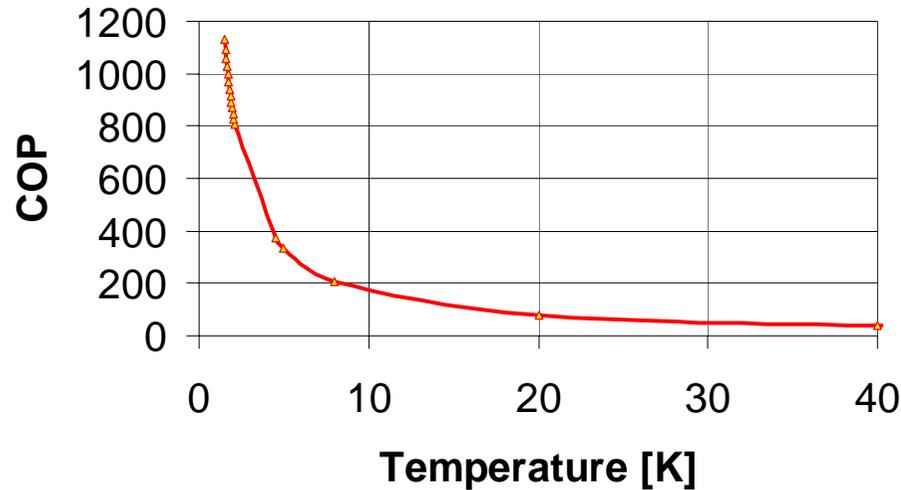
Some Refrigerator COPs

1 W useful refrigeration at 2 K = 870 W Primary Power !!!

Refrigeration Temperature	Carnot $1/\eta$ IDEAL WORLD	XFEL-Spec REAL WORLD	% Carnot
2 K	149	870	17
5 K	79	220	36
40 K	7	20	33

Coefficient of Performance

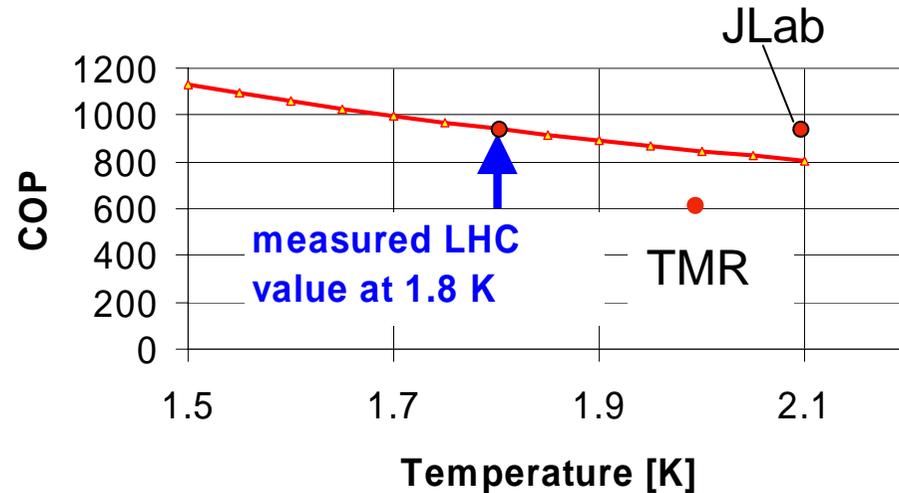
COP vs T



$$\text{COP}_{\text{real}} = 1 / (K * \eta_{\text{CARNOT}})$$

$$\eta_{\text{CARNOT}} = T / (300 - T)$$

K = 0.176 (from latest LHC measurements at 1.8 K)



Why do we care about COPs ?

Cooling at liquid helium temperatures $T < 5 \text{ K}$ is very expensive !

Large SRF facilities (JLAB,SNS, ERLs, XFEL,ILC.....) need Megawatts of primary power supply.

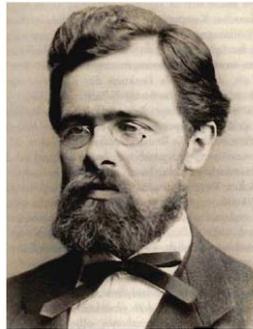
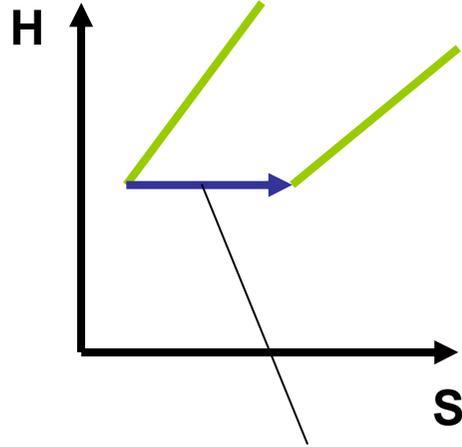
Excellent thermal insulation is mandatory !

Already at about $T > 40 \text{ K}$ the situation is much more relaxed !

-> Direct heat loads as much as possible to temperature levels above 40 K (Radiation, HOM-loads, solid state thermal conduction.....)

Some Helium Refrigerator Cycles

Simple LINDE cycle



Carl von Linde 1842-1934

Ideal Joule-Thomson Expansion =
Isenthalpic Expansion $\Delta H=0$

Compressor

*Will this work
for Helium ?*

HEX

Heat Exchanger



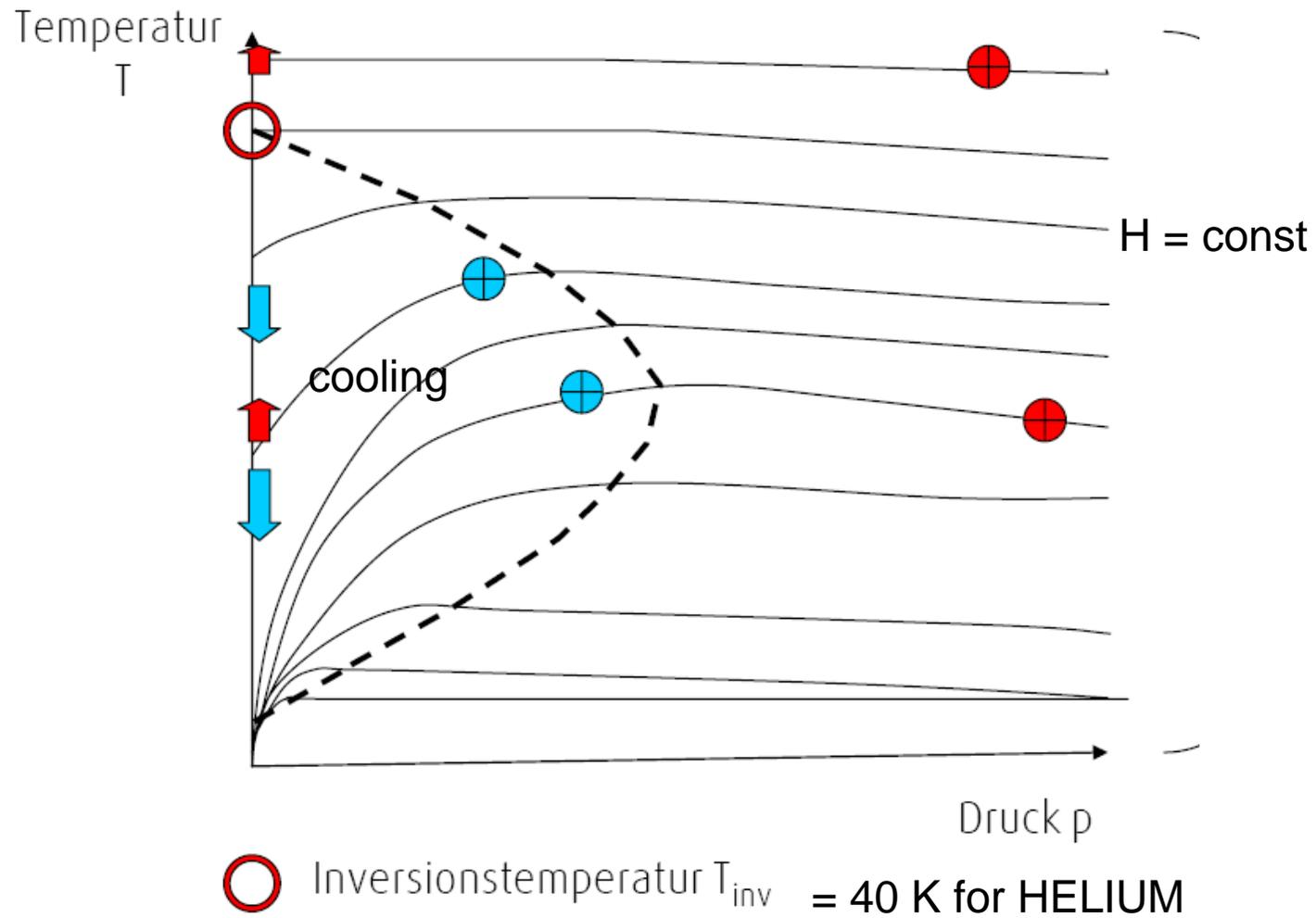
JT

Joule-Thomson
Valve

load

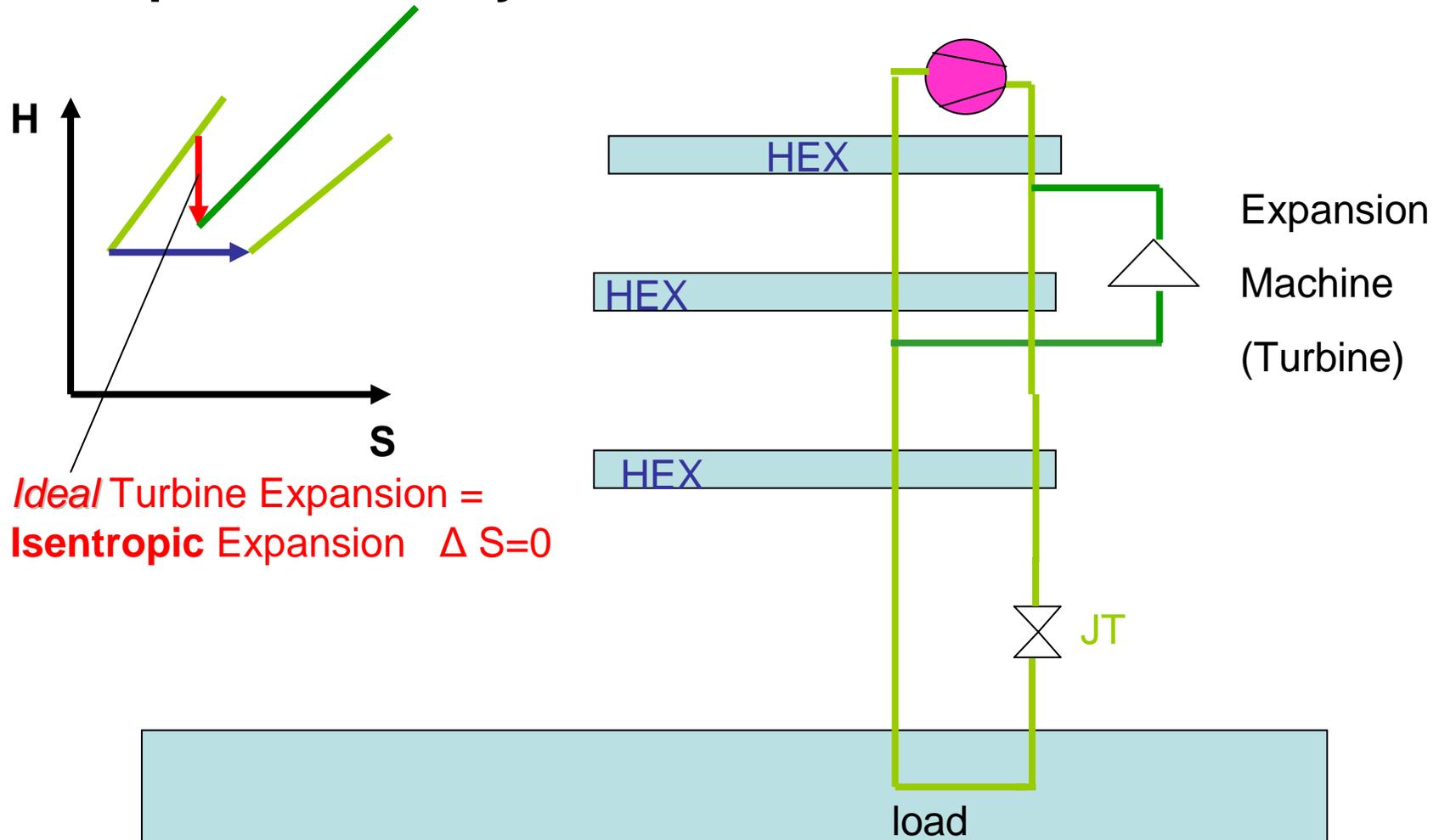


Joule-Thomson Expansion: Inversion Curve



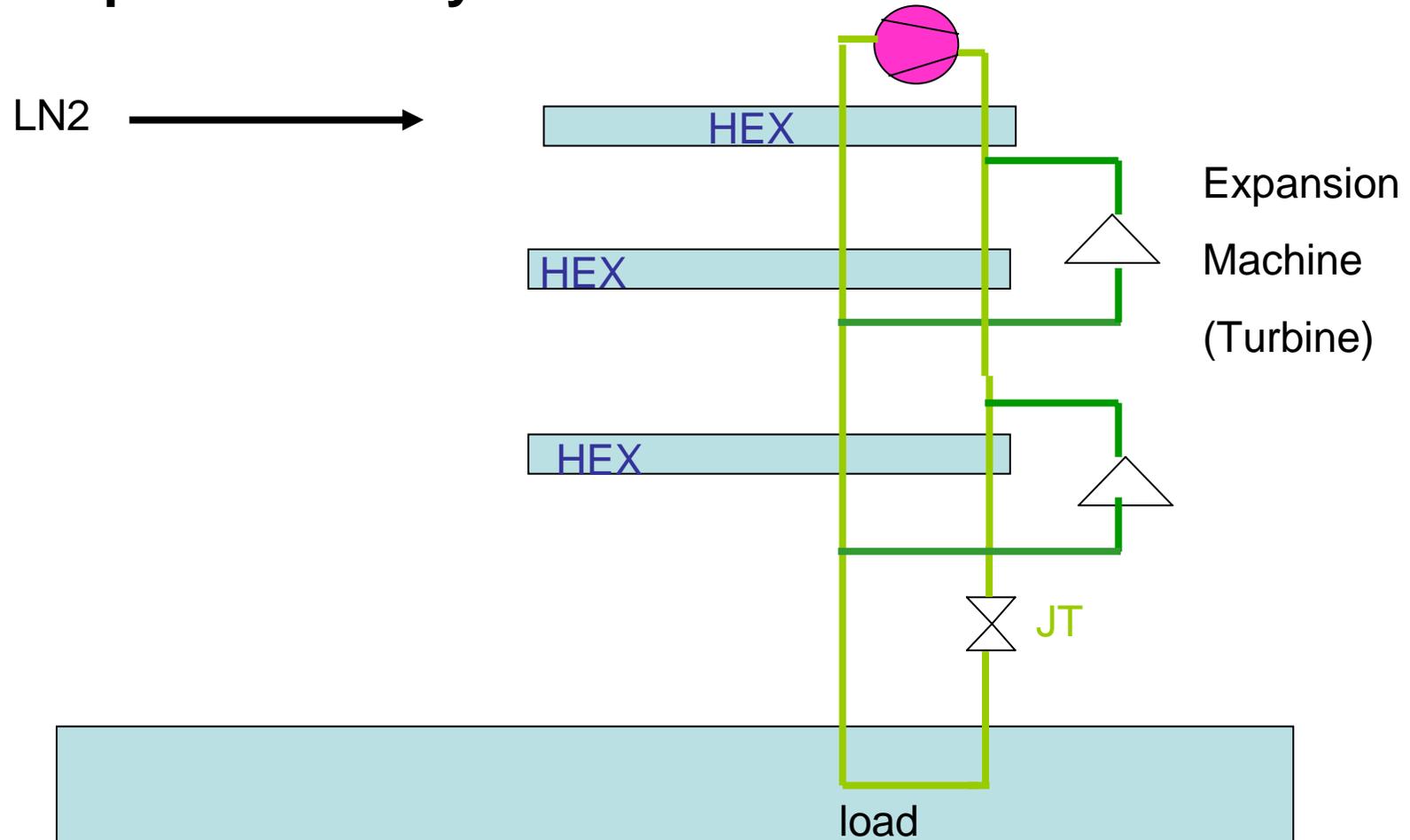
Some Helium Refrigerator Cycles

Simple Claudet Cycle



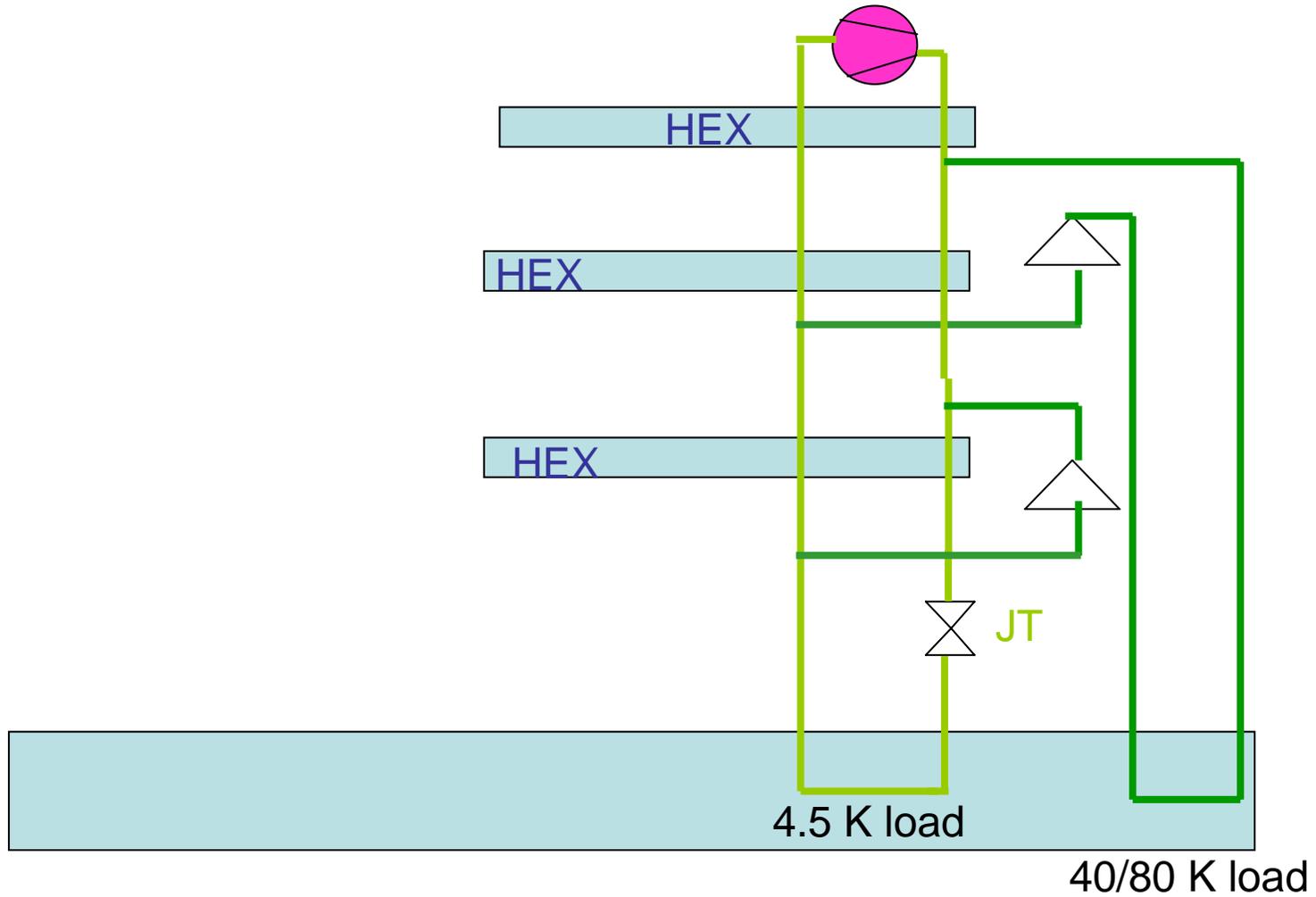
Some Helium Refrigerator Cycles

Simple Collins Cycle

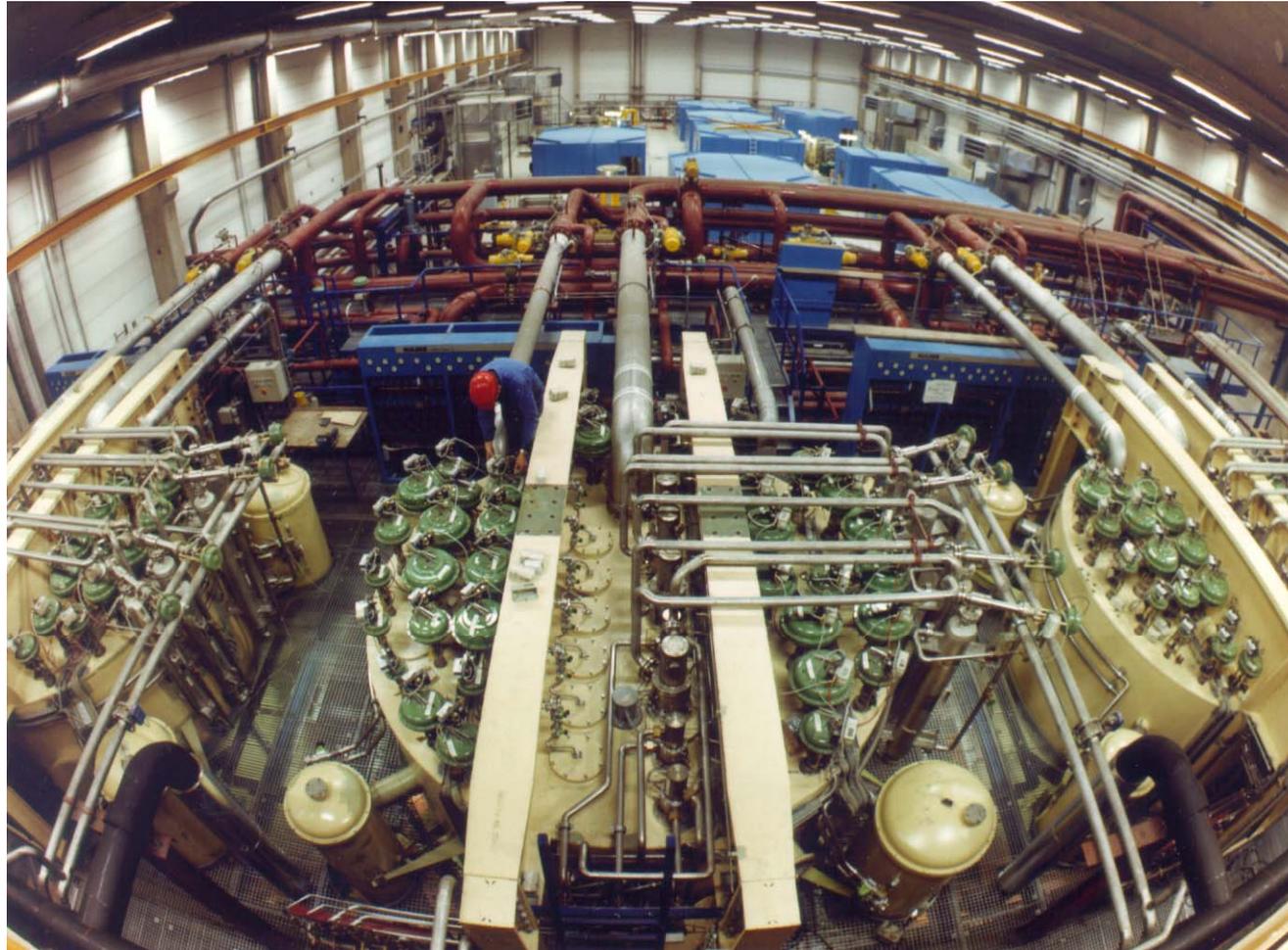


Some Helium Refrigerator Cycles

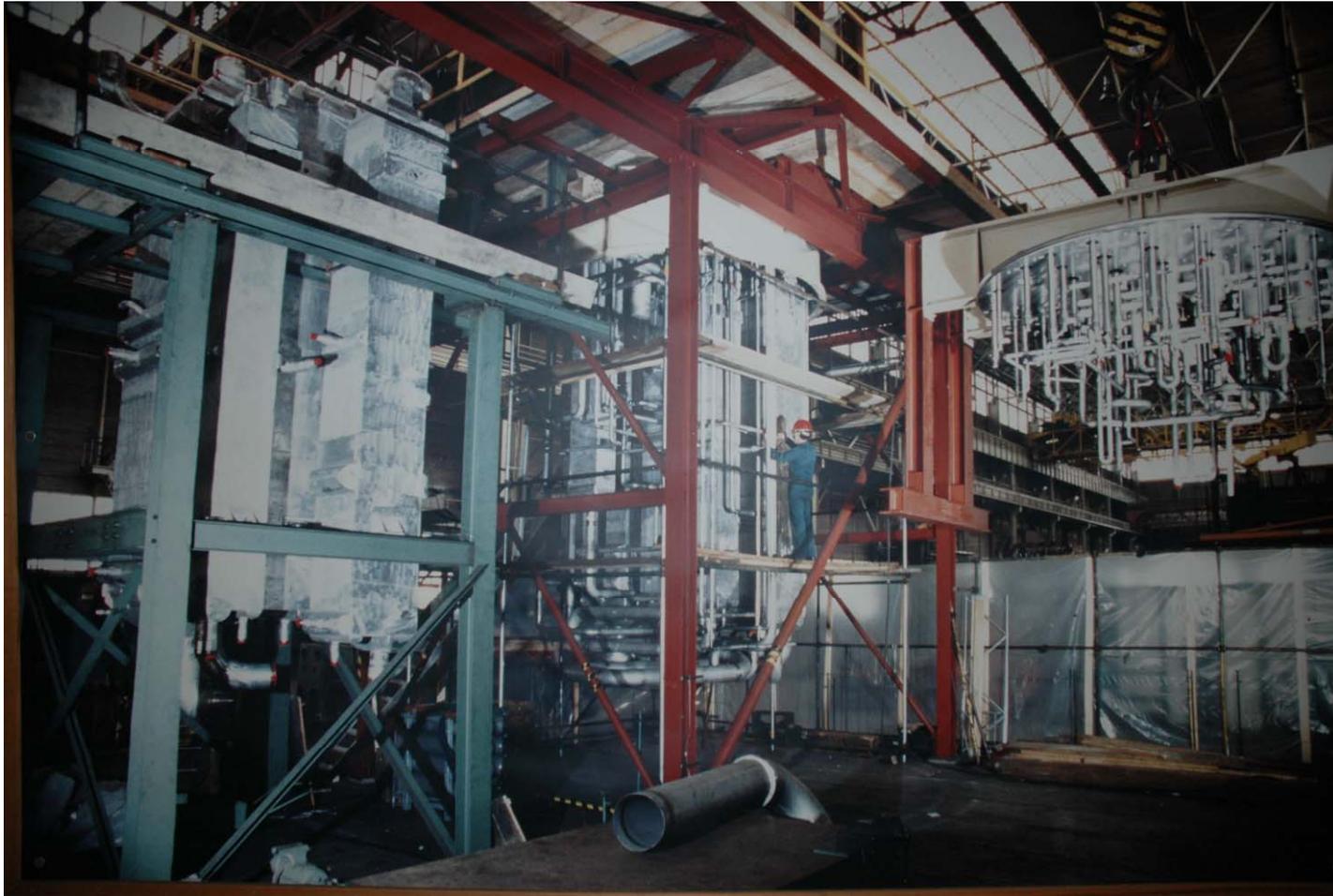
Simplified 4.5 K Helium Refrigerator + Shield Cooling



Example: HERA Cryo Plant

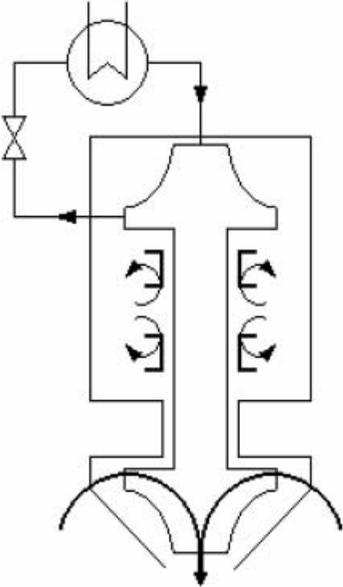
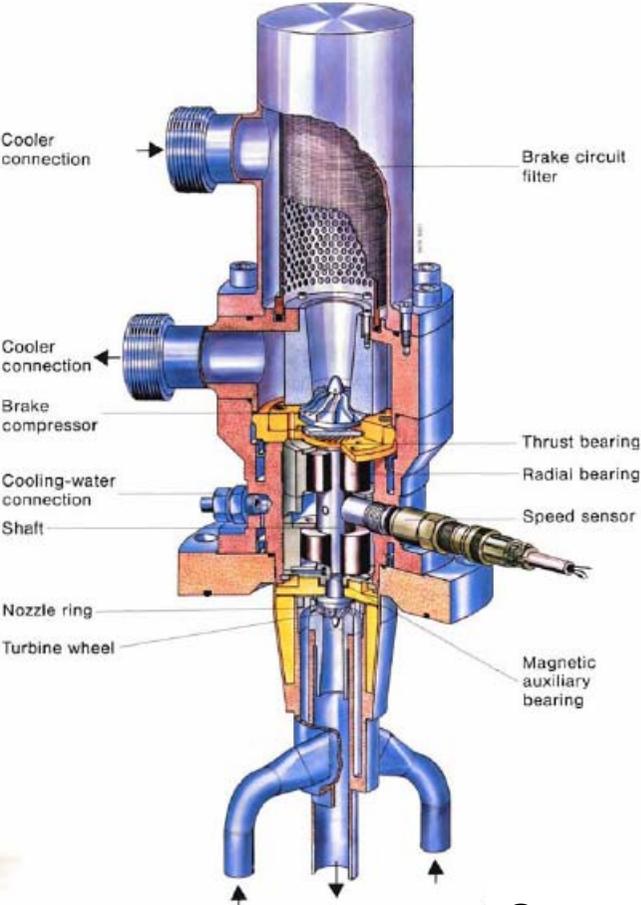


Inside HERA Cold Boxes



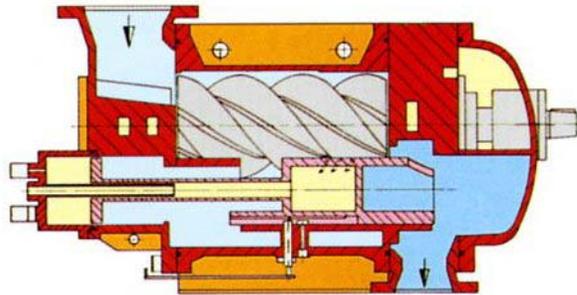
Cryogenic Turboexpander

Cryogenic turboexpander
Self-acting gas bearing system

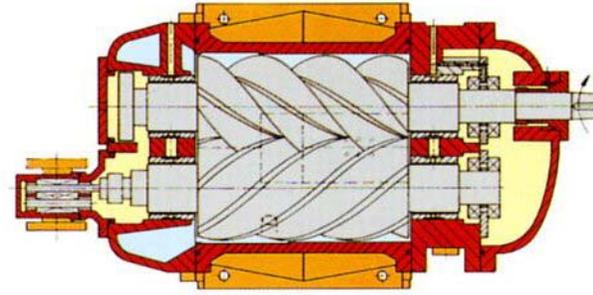


Source: LINDEKRYOTECHNIK AG

Screw-Compressors



Längsschnitt: Ansicht von der Seite.



Längsschnitt: Ansicht von oben.

Abb. AERZENER Maschinenfabrik, Aerzen

Source:
AERZEN

B bis Δp 8 bar
 Ansaugvolumenströme von 500 m³/h bis 9400 m³/h
 Stufenlos regelbar zwischen 100 % und 10 %
 Betriebsüberdruck max. 25 bar (GG 25)
 40 bar (GG 40)
 Betriebsunterdruck - 0,999 bar

Verdichtungsorgan

Ansauger

Verdichten

Verdichten

Ausschieben

① Rotoren
 ② Radial-Gleitlager
 ③ Axial-Wälzlager
 ④ Kapazitätsschieber

⑤ Hydraulikkolben
 ⑥ Ölpumpe
 ⑦ Antriebszapfen

Aerzener Maschinenfabrik GmbH
 Postfach 7-9 · Reherweg 28 · D-3251 Aerzen 1 · Telefon 05154/810 · Telex 92247

HERA-Screw Compressors



LP + MP

HP

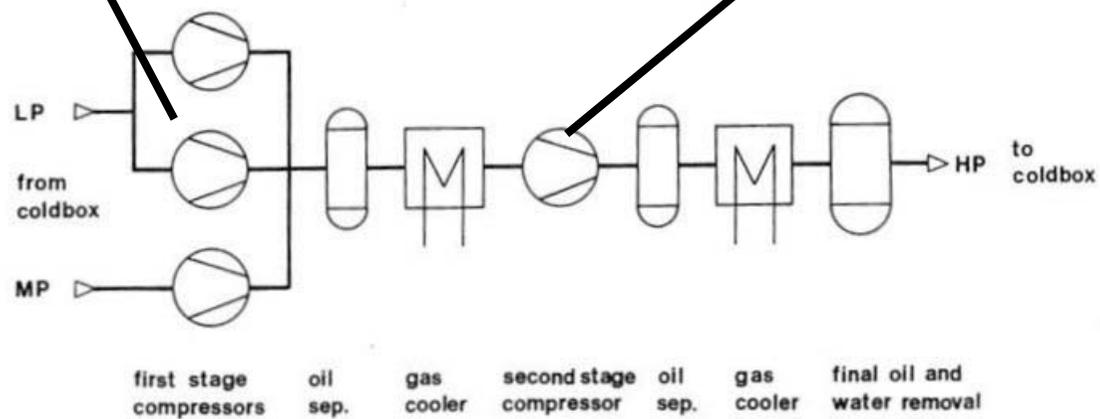
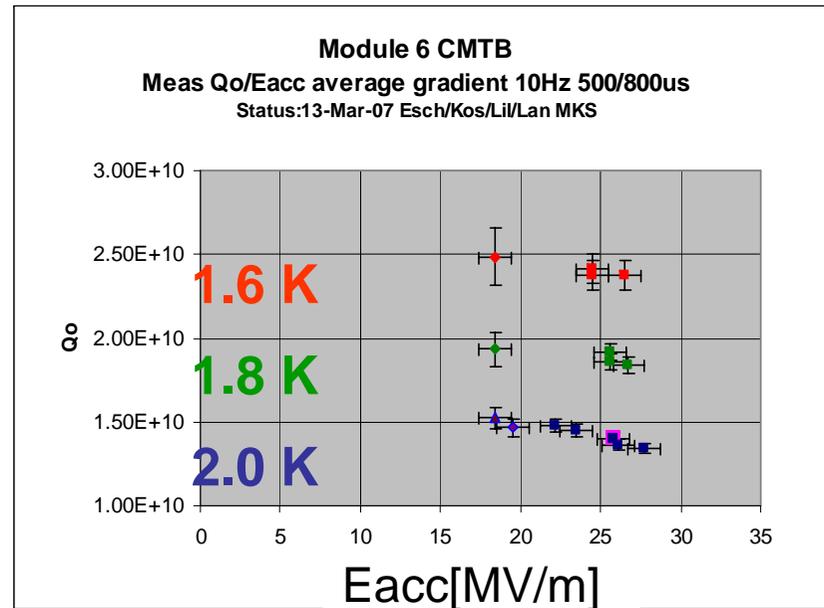


Fig. 2. HERA refrigerator: compressor flowsheet

,Choice of operation temperature for a sc cavity‘

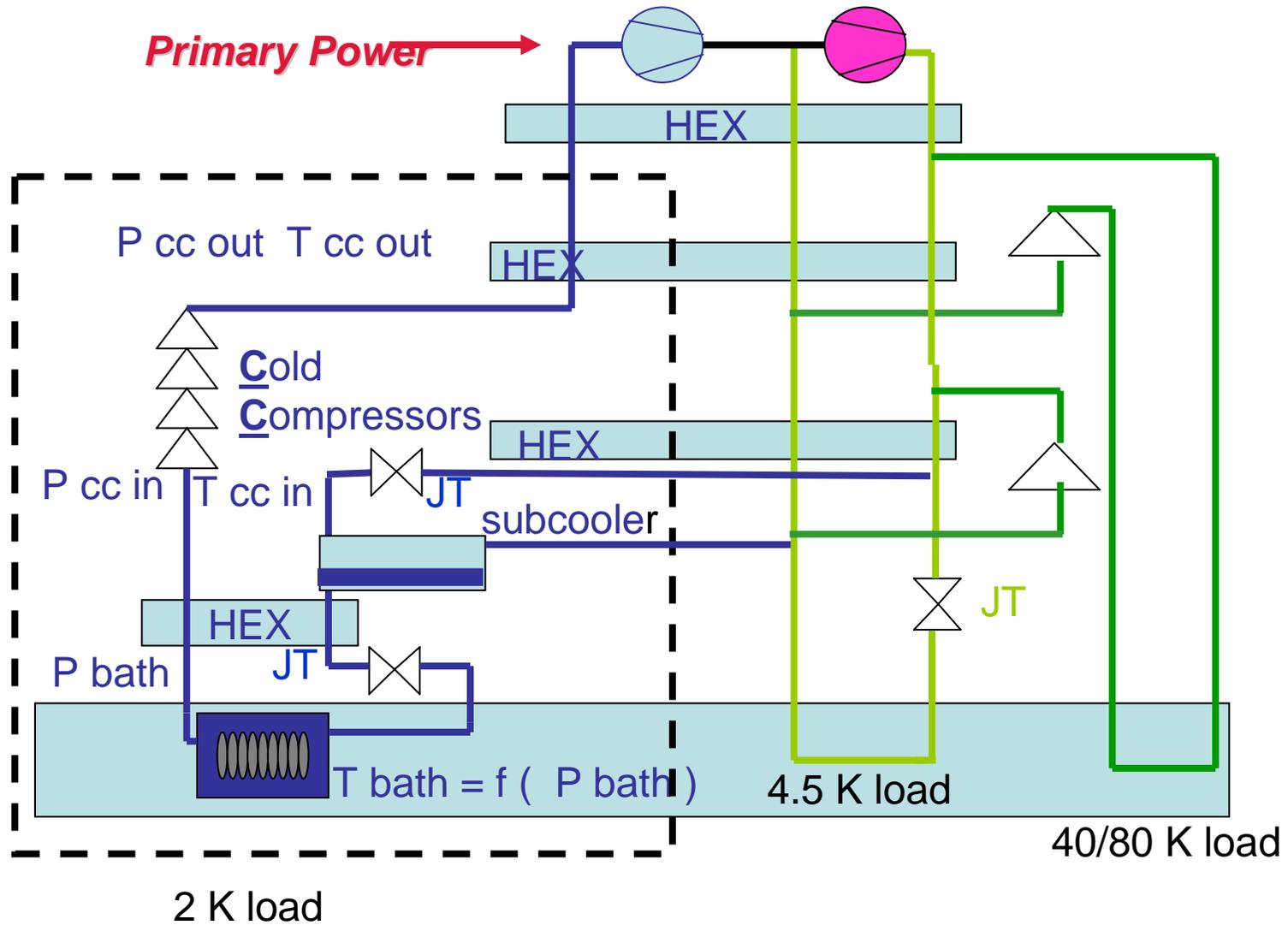
Qo



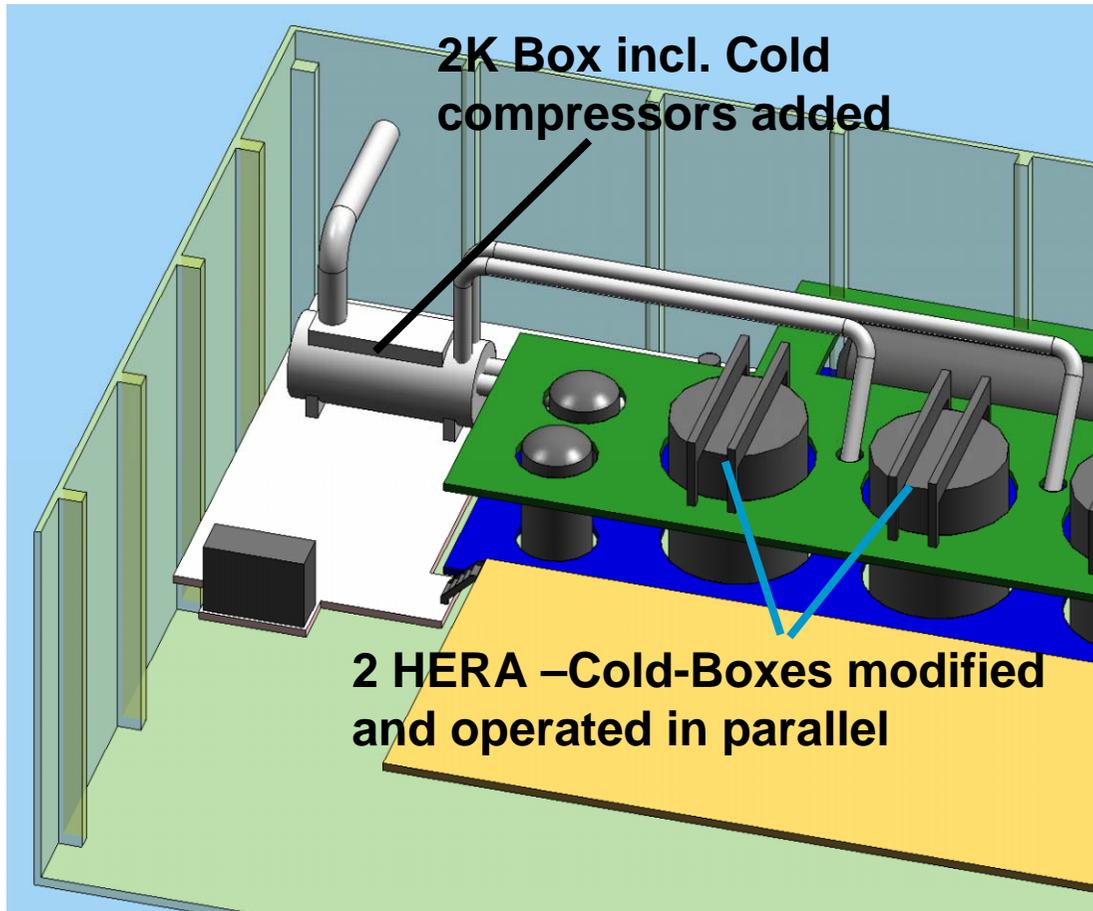
(Courtesy of R.Lange et al. DESY MKS)

Qo versus Eacc measurement for a
complete TTF-cryomodule type III
(similar to XFEL-prototype)

Simplified 2 K Helium Refrigerator + Shield Cooling

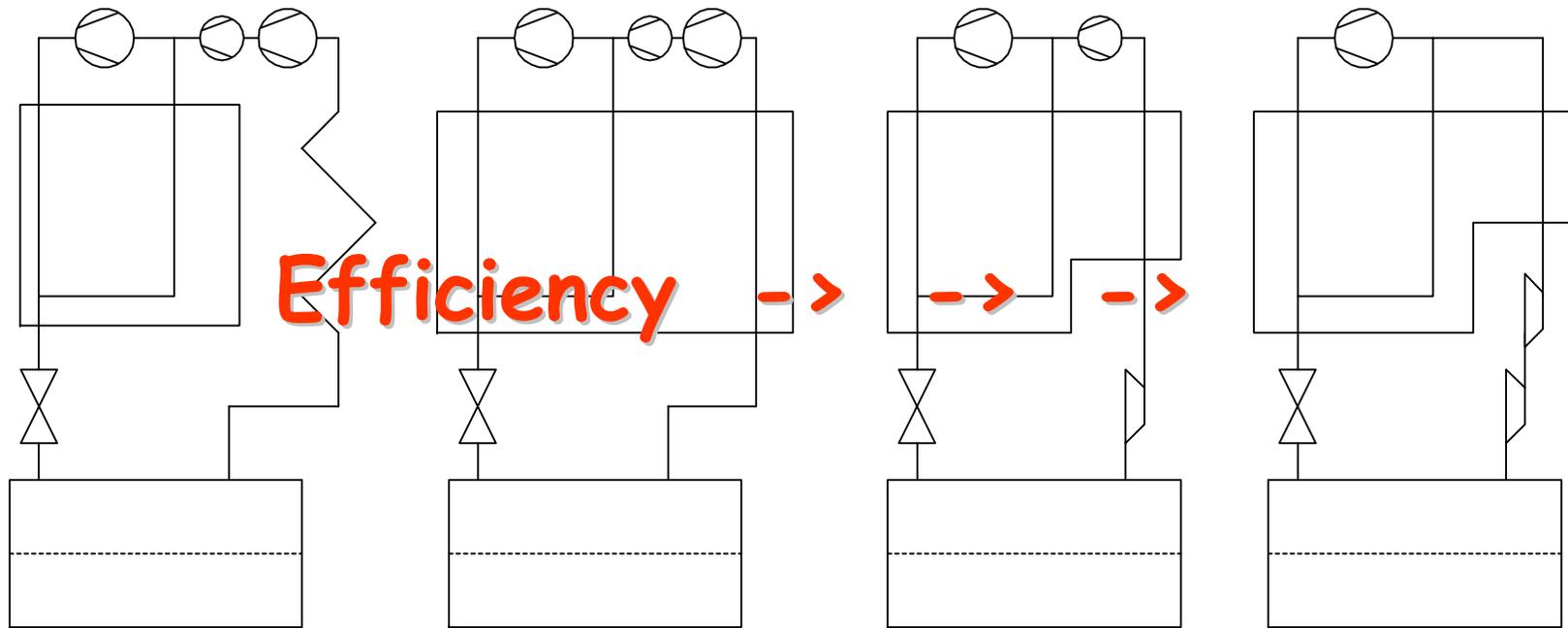


The 20-year old HERA cryogenic plant will be up-graded to the 2 K- XFEL-cryogenic plant



Source: LINDE KRYOTECHNIK AG

Options to Produce Temperatures below 4.4 K, i. e. Evaporation of Helium at Reduced Pressures



A

Only the heat of evaporation of the helium is utilized.

B

The low pressure stream is warmed up in a heat exchanger inside the refrigerator cold box.

C

The cold low pressure stream is precompressed by a coldcompressor.

D

The precompression is realized by several stages of cold compression.

Option A example: warm helium compressors for FLASH- linac/TTF supply at DESY

4 rotary vane pumps + 3 stages of roots blowers
10 g/s helium flow compression: 10 mbar -> 1.05 bar
(two identical sets of compressors for linac and TTF)



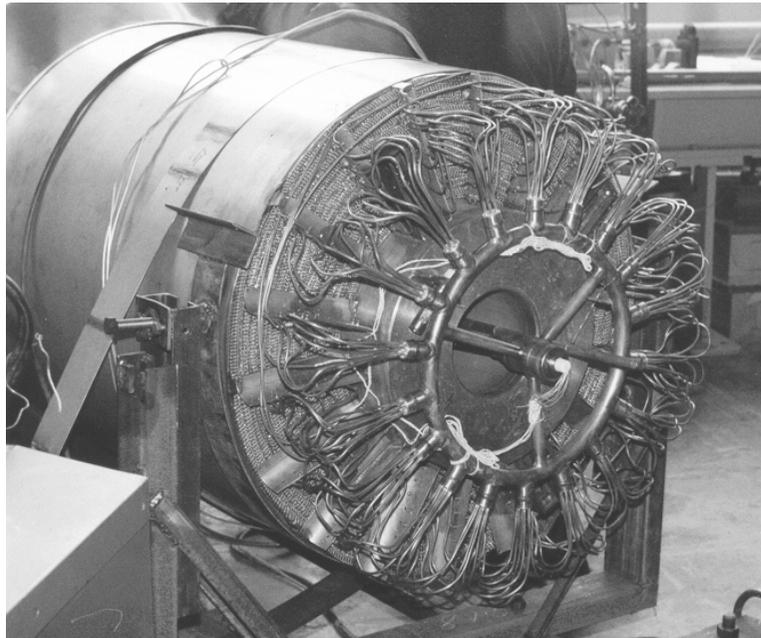
Option B: use of heat exchanger

Example: FLASH linac at DESY

External low pressure heat exchanger (IHEP,Russia)
counter-flow heat exchanger:

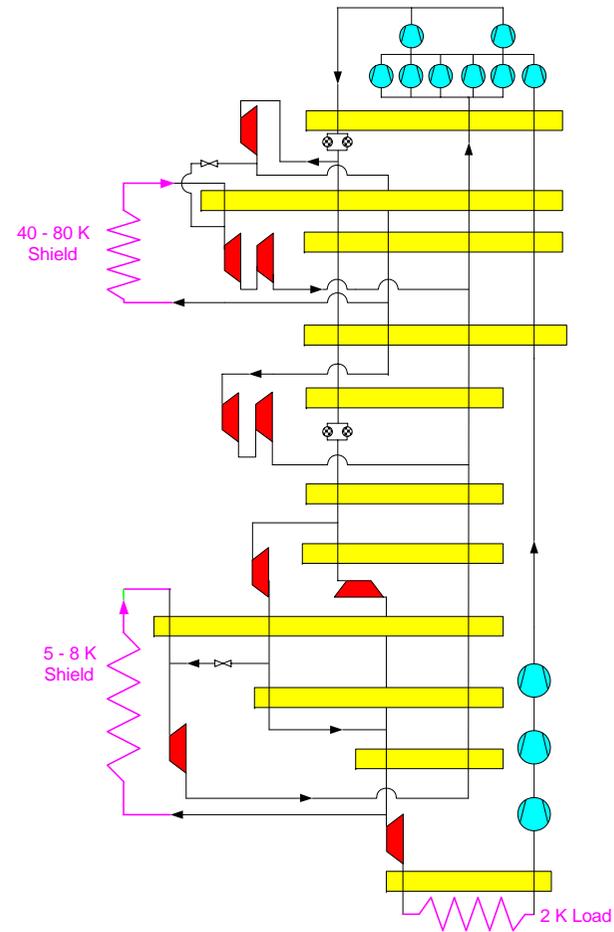
3,5 K / 31 mbar -> 280 K / 29 mbar

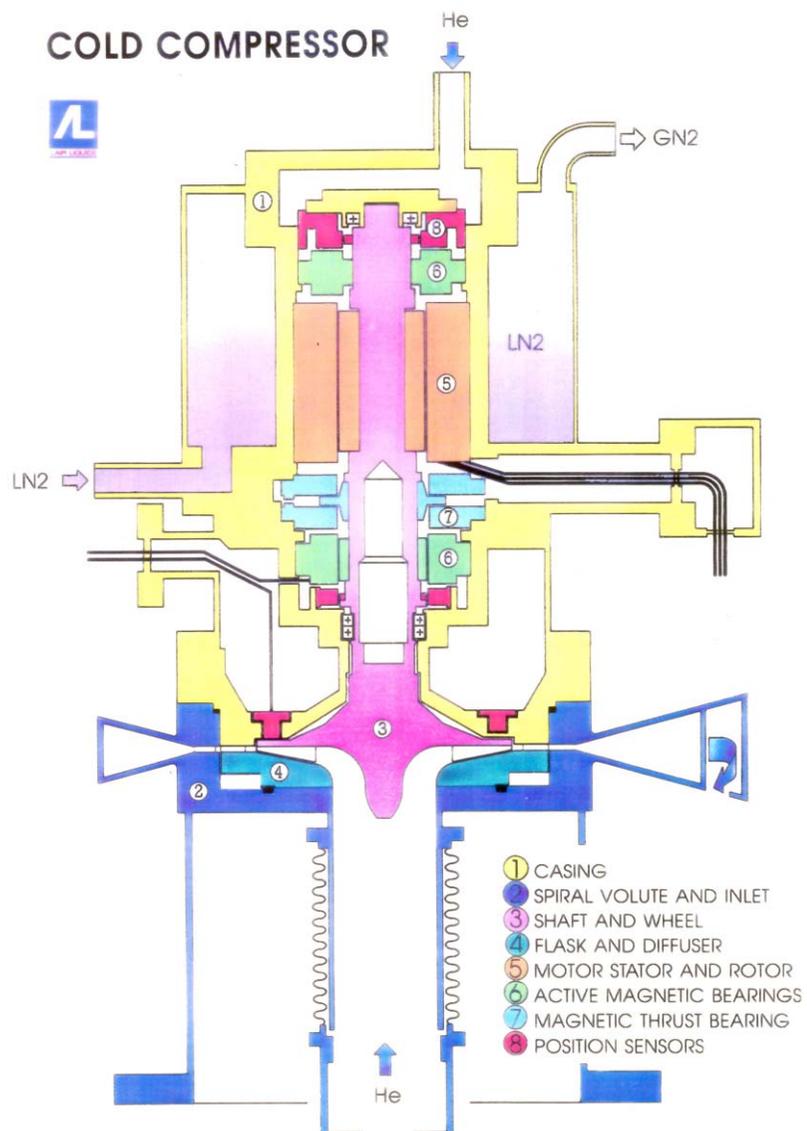
7,5 K / 12 bar <- 300 K / 12 bar



Option C/D Example: TESLA Model Refrigerator

- layout by TU-Dresden
- advice from CERN
- discussion with industry
 - component number and size,
flow rates, power consumption
- flow scheme
- 8 screw compressors
- 9 turbines
- 3 cold compressors





Example of a cold compressor with active magnetic bearings used at Tore Supra, CEBAF and Oak Ridge

Source: Air Liquide

Cold Compressor Cartridges of 2.4 kW @ 1.8 K Refrigeration Units

IHI-Linde



Cold compressor impeller

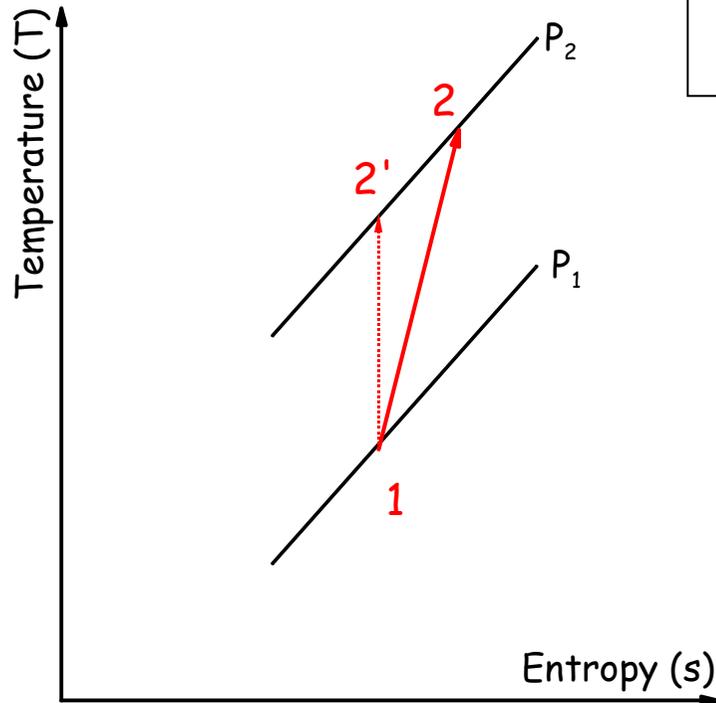


1st stage

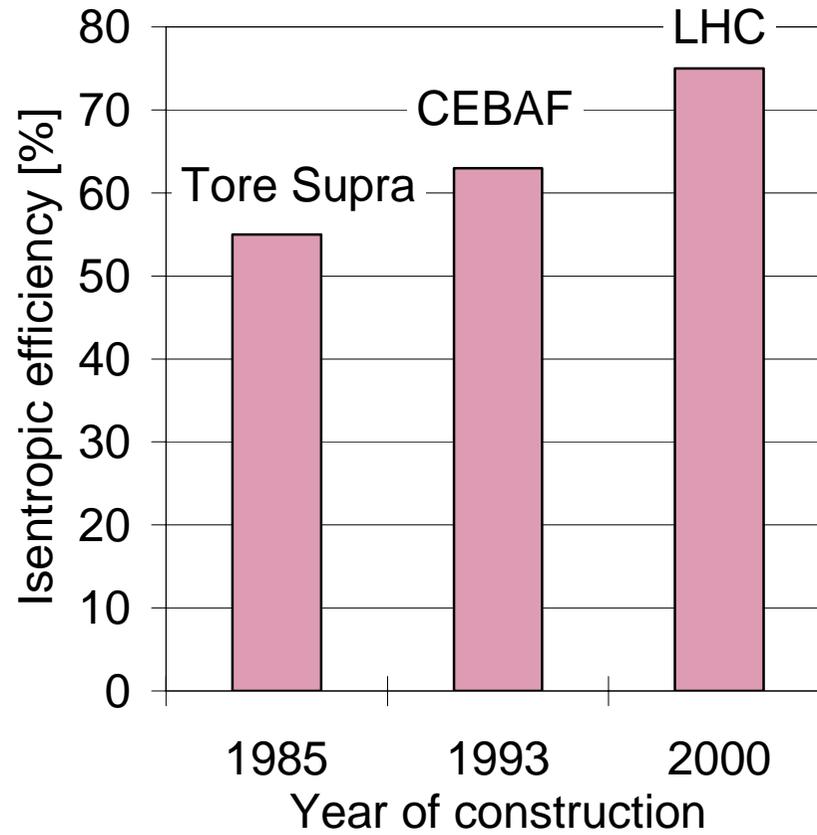


The four-stage LHC cold compressors

Development of the Efficiency of Cold Compressors



$$\eta_{is} = \frac{H_{2'} - H_1}{H_2 - H_1}$$



,Quantum Properties' of Matter at low T

Many physical effects can be characterized by a typical Excitation Energy ΔE

The probability of excitation is about $\sim \text{EXP}(-\Delta E / k_B T)$

For $T \rightarrow \infty$ all states are excited.

For $T \rightarrow 0$ condensation in the ground state

$\Delta E =$ binding energy \rightarrow condensation of matter , **liquifaction of gases**

$\Delta E = \hbar \omega$ phonons in solids \rightarrow **specific heat, thermal conductivity**

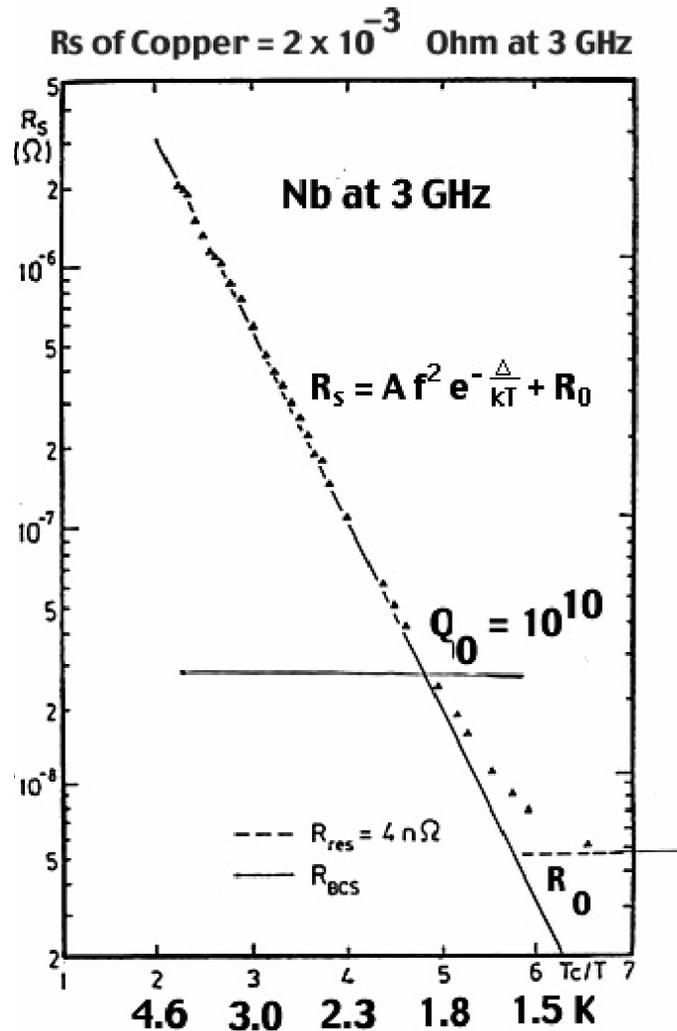
$\Delta E =$ superconducting energy gap \rightarrow **superconductivity**

$\Delta E =$ band gap of semiconductors \rightarrow **electrical resistance**

Other effects are not disturbed by thermal energy at low T like:

Helium II phenomena (Bose condensation), **Kapitza-Effect**,...

That's why we have this SRF workshop.....

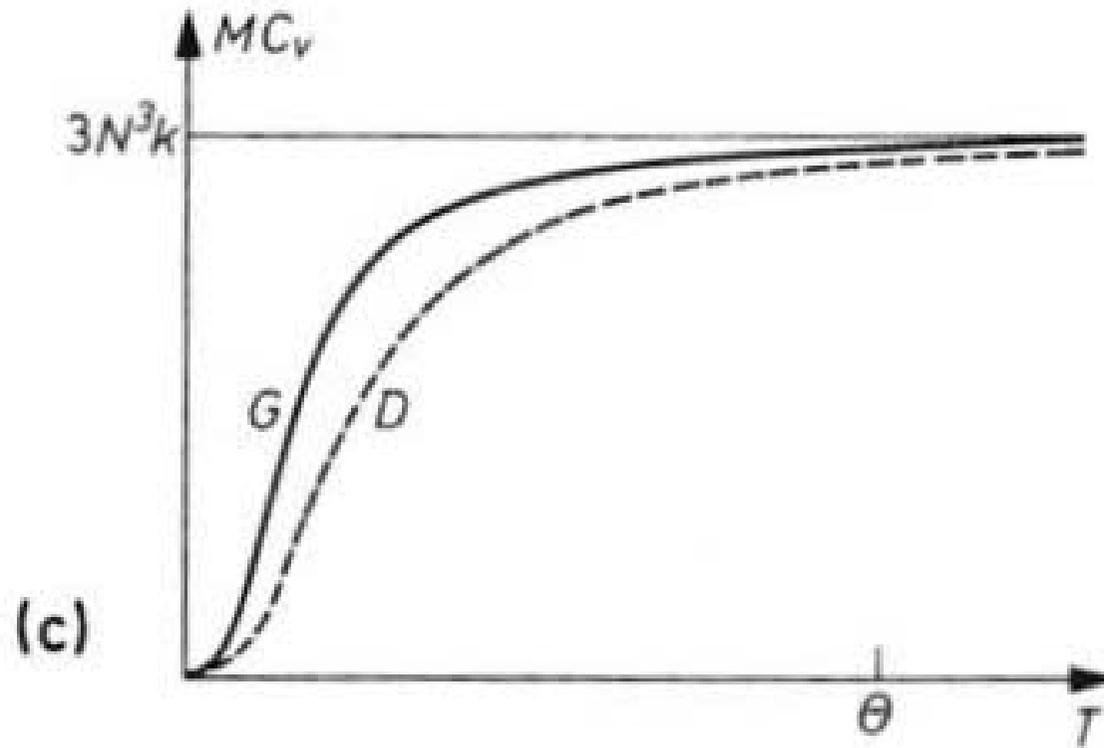


Measurement of the superconducting surface resistance at 3 GHz

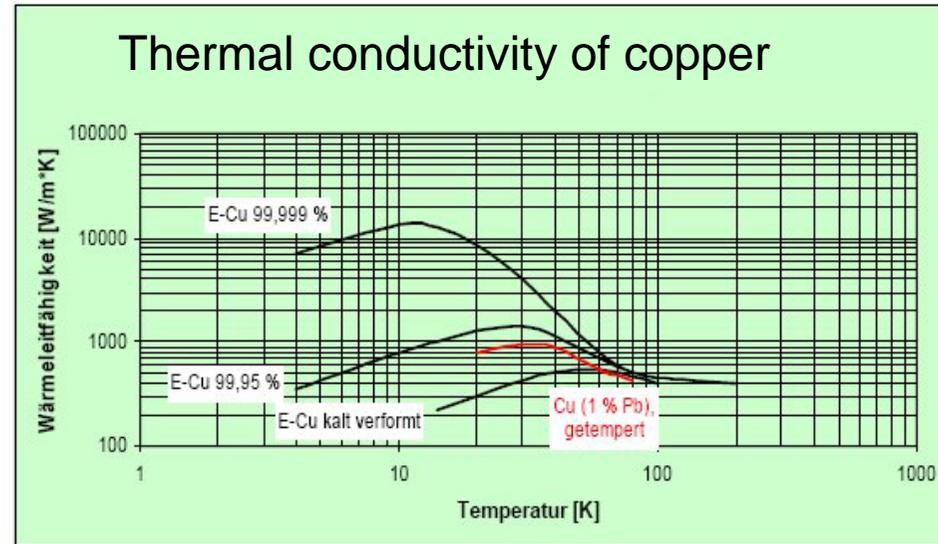
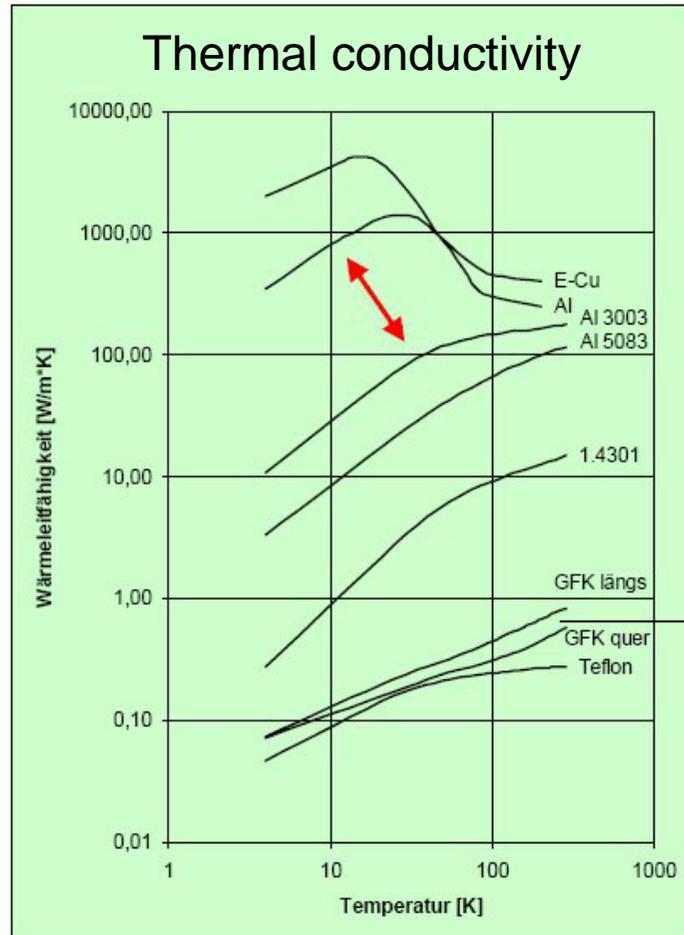
Nb/Cu : reduction of R_s by nearly 6 orders of magnitude

Quantum Properties of Matter at Low Temperatures

Specific Heat of Solids



Thermal Conductivity of Solids at Cryogenic Temperatures



Glas fiber re-inforced epoxid

Thermal contraction of solids

Thermal Stress

$$\Delta L/L$$

Plastics > 2%

Steel 0,3%

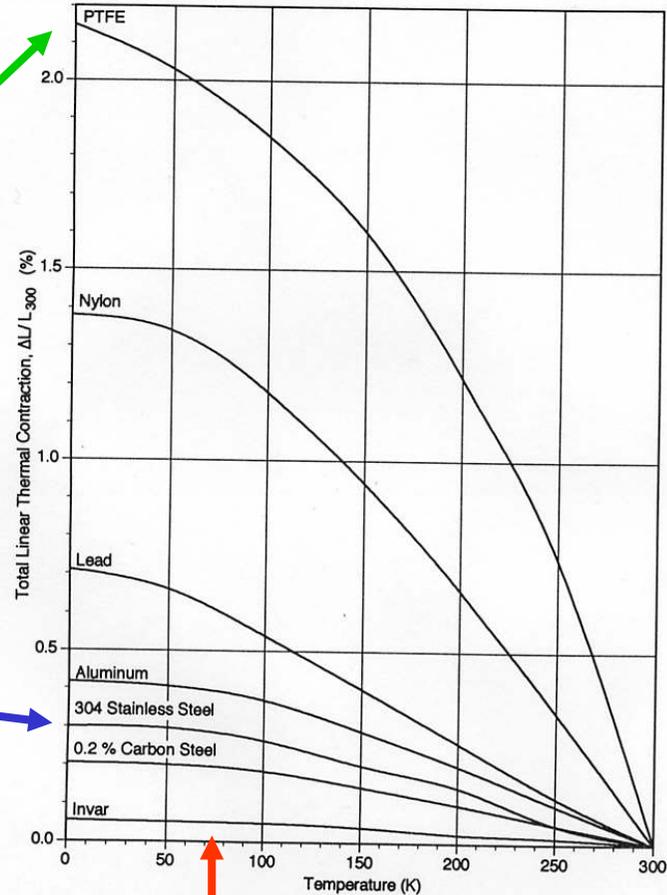
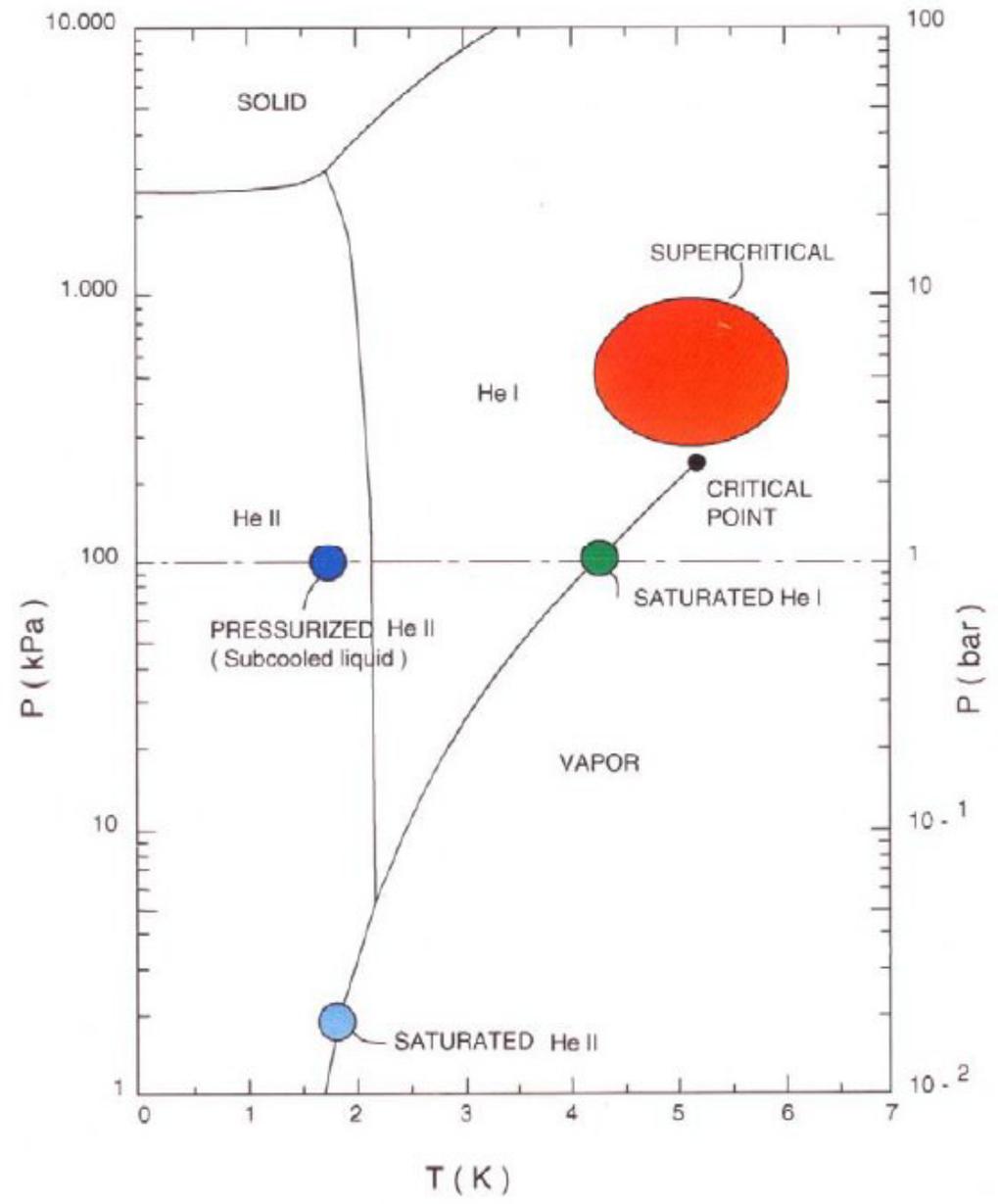


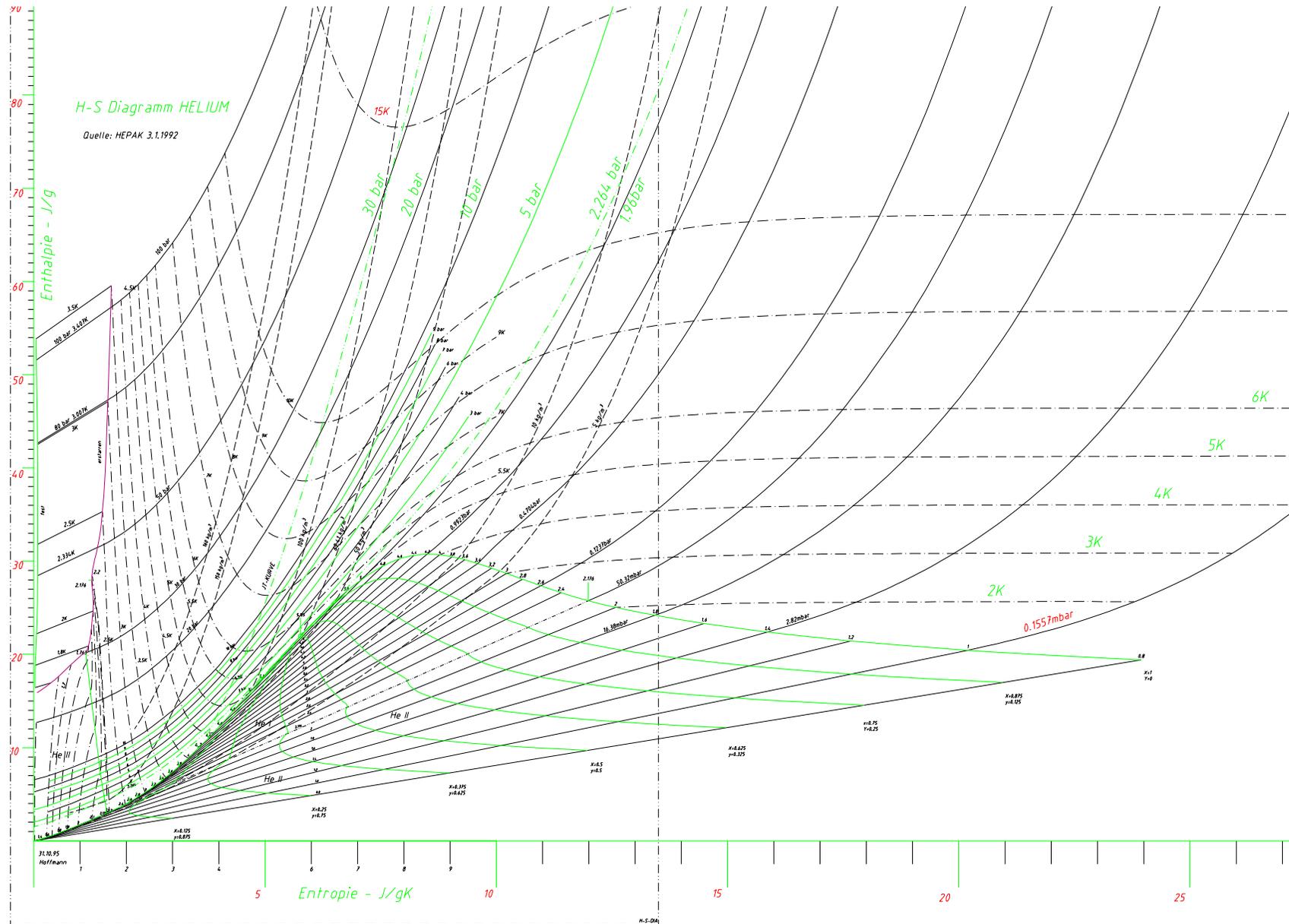
Fig. 4.2. Plots of linear thermal contraction of some common materials as a function of temperature,³ showing the total contraction at a given temperature as the temperature is lowered from 300 K to that temperature. PTFE = Polytetrafluoroethylene.

77K

PHASE DIAGRAM OF HELIUM

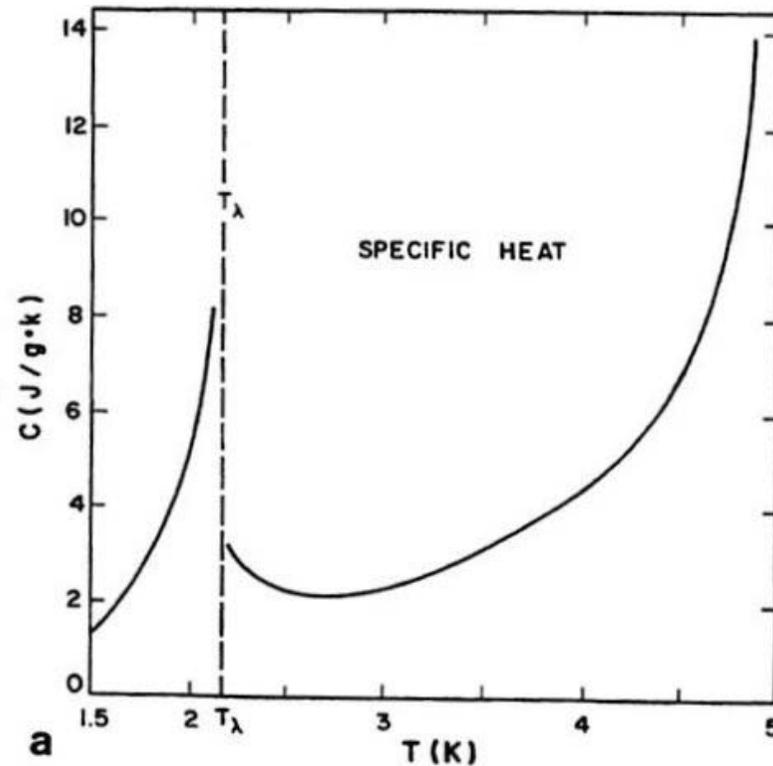


Other View: H-S-Diagramm of Helium (Source: HEPAK)



Quantum Properties of Matter at low T

Specific Heat of liquid HELIUM

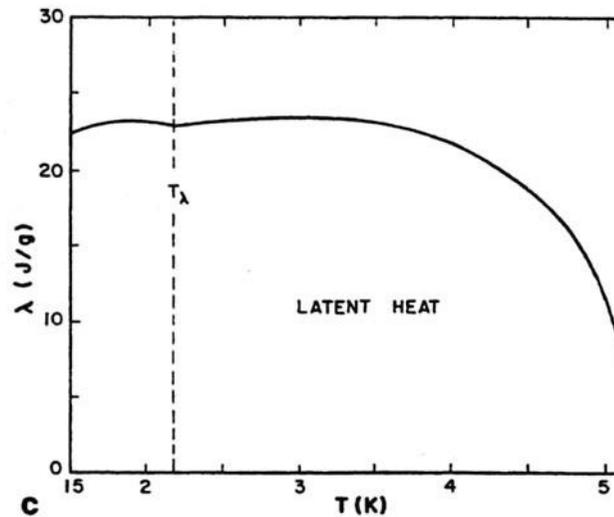


a. Specific heat of liquid helium at saturated vapor pressure.

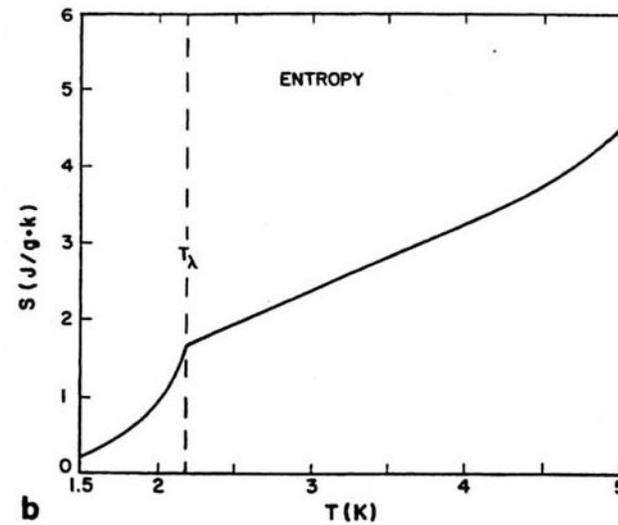
**Much larger
than specific
heat of solids at
these
temperatures !**

Quantum Properties of Matter at low T

Latent Heat and Entropy of liquid HELIUM



Latent heat of vaporization of liquid helium.

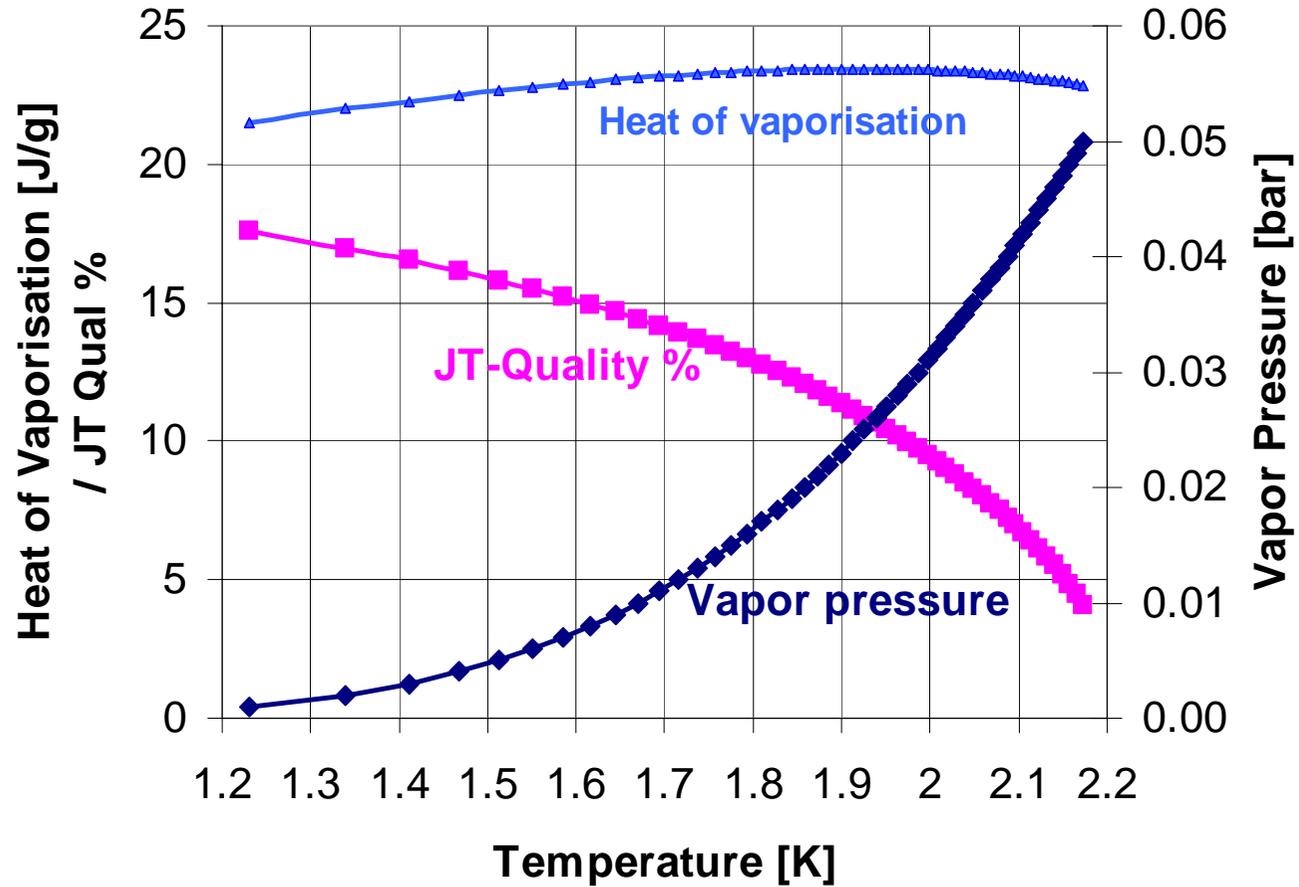


Entropy of liquid helium at saturated vapor pressure

**Phase Transition HE I \rightarrow HE II ,second kind' phase transition
(no latent heat)**

Helium II parameters = f(T)

Helium Parameters vs. Temperature



Definition of Lambda max in a HEII bath

Heat conductivity in Hell

$$q^{**m} = f(T) * dT/dx$$

T-Temperature, x-length
m ≈ 3

$$f(T) \text{ Germany} = f^{**(-1)}(T) \text{ USA}$$

$$q \text{ max} * L^{**1/3} = \left[\int_{T1}^{T2} f(T) dT \right]^{**1/3}$$

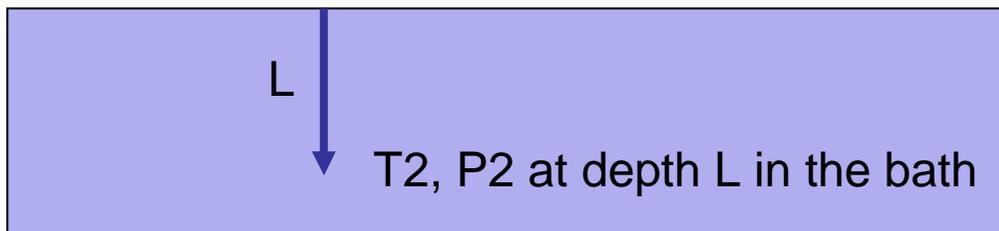
T1 = F (P1) Temperature function of vapour pressure

T2 = F (P1 + Δ P)

Δ P = ρ * L * g ρ = density of liquid g=9.81 m/s²

L= depth in bath

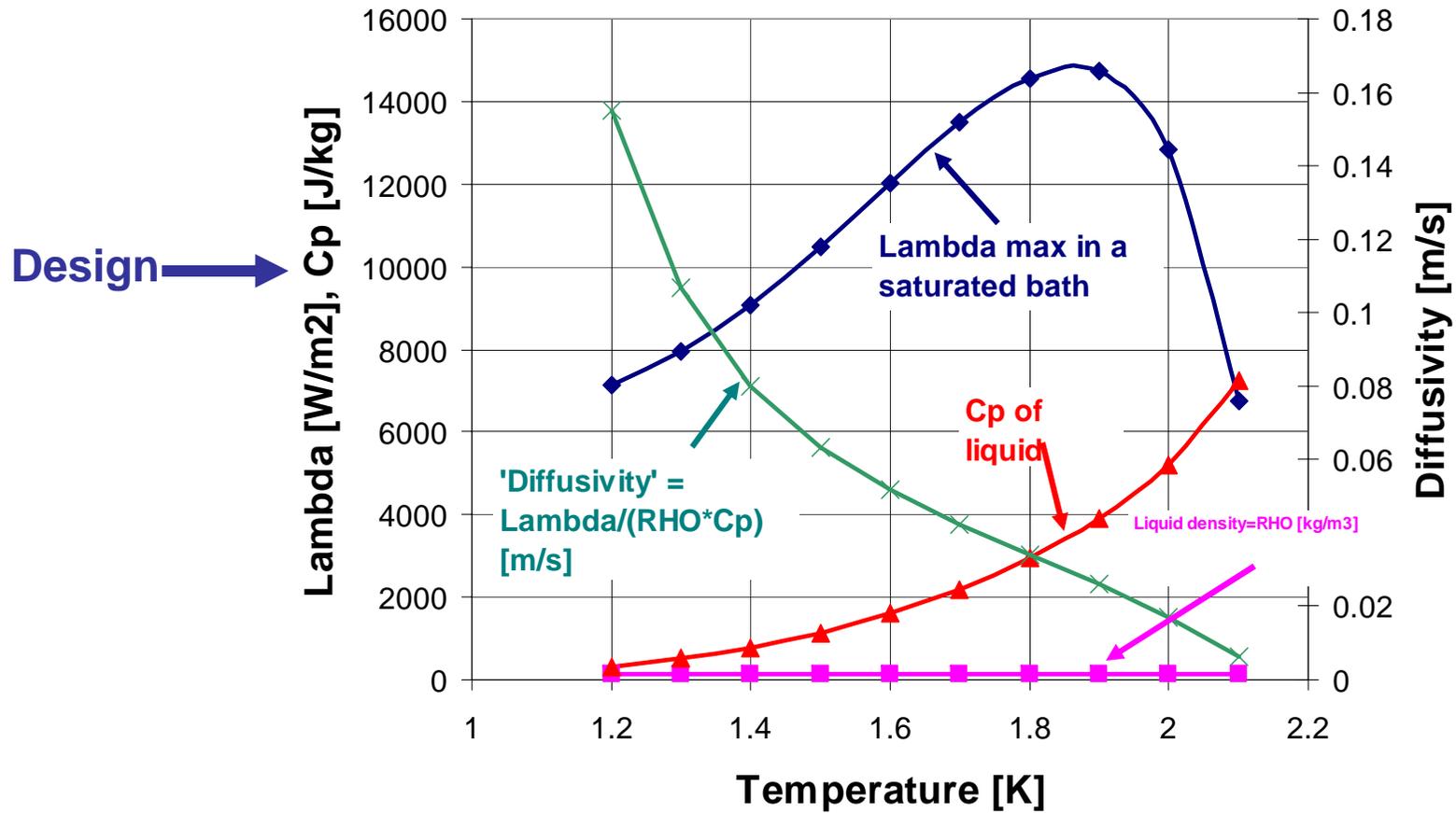
T1, P1 at liquid surface



T2 must not be exceeded to avoid bubbles !

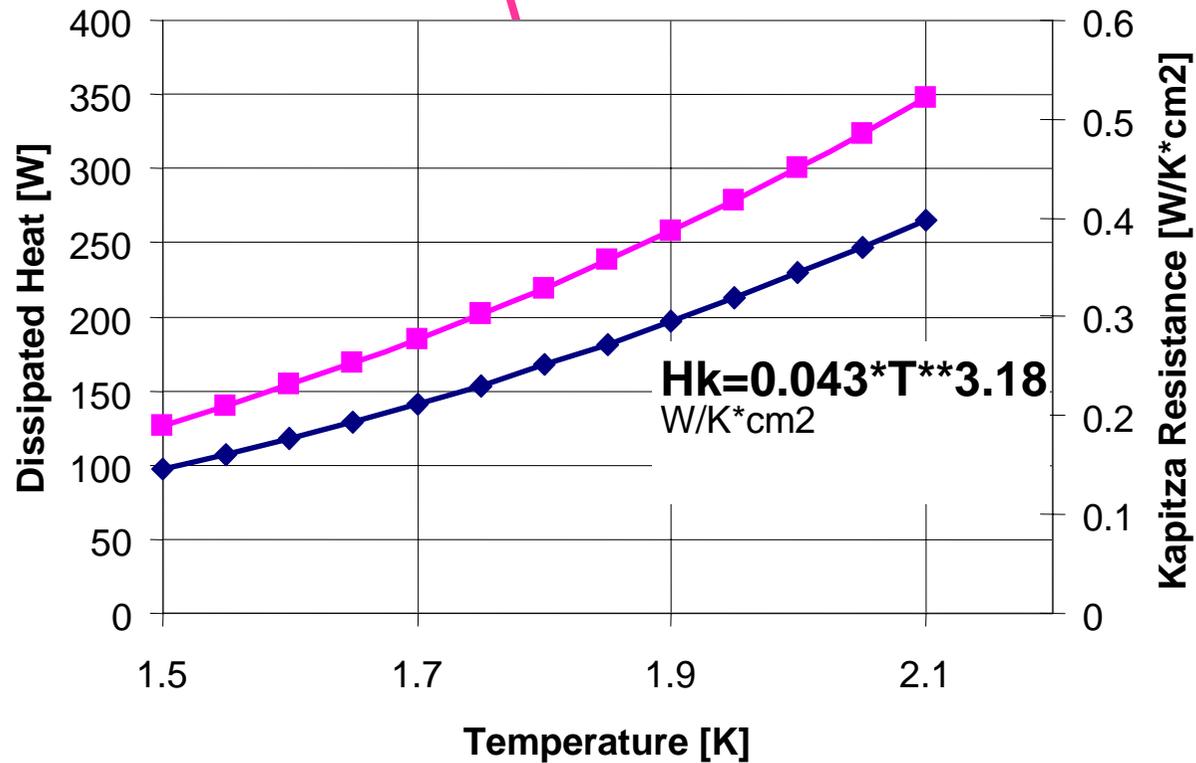
Helium II parameters = f(T) (cont.)

Lambda, Cp, Diffusivity, Density of HELIUM II



Kapitza Heat Transfer Solid Surface to Helium II

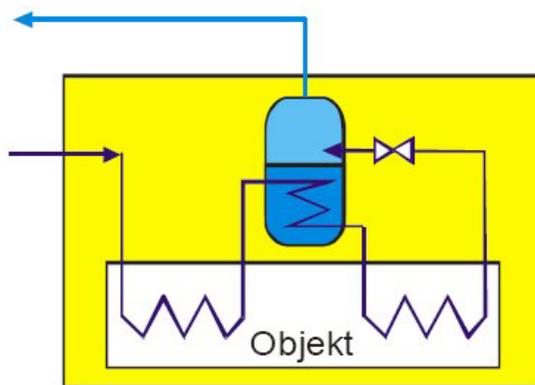
Heat transfer at the surface of one
TESLA cavity $\Delta T = 100$ mK



For
Niobium

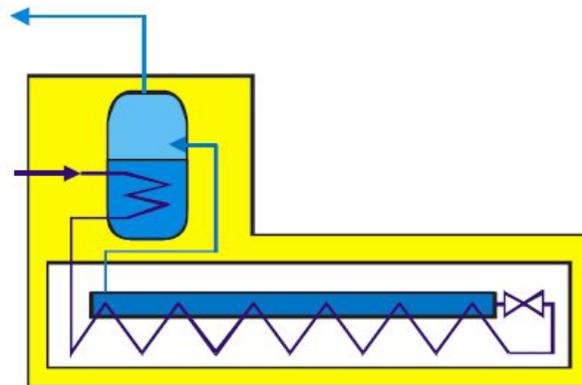
Some Cooling-Cycles:

Forced 1-phase Helium I Cooling



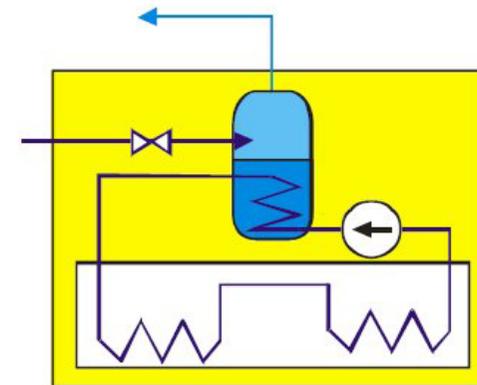
SC Quadrupoles in
TTF-Cryomodules

+ = simple
- = large mass flow
excess liquid



HERA Accelerator SC
Dipoles

++ = homogeneous
cooling of sc coils at
constant temperature



HERA Accelerator
Lumi-up-Grade SC
Magnets

+ = no excess liquid
- = large mass flows
extra pump

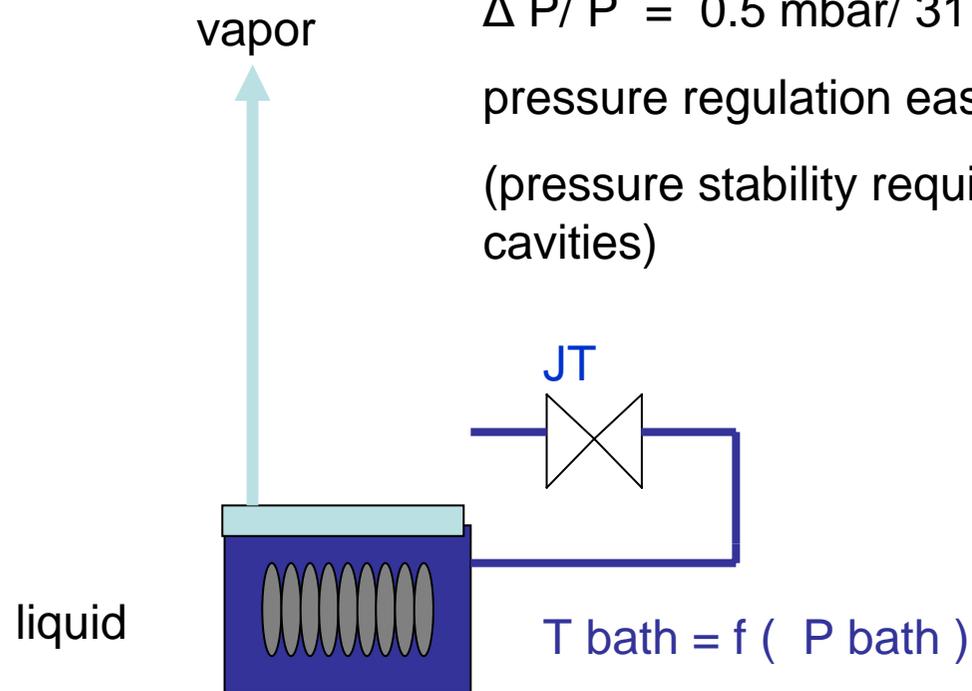
Some Cooling cycles: Bath cooling

Advantages: very simple

$$\Delta P / P = 0.5 \text{ mbar} / 31 \text{ mbar} = 0.016$$

pressure regulation easy

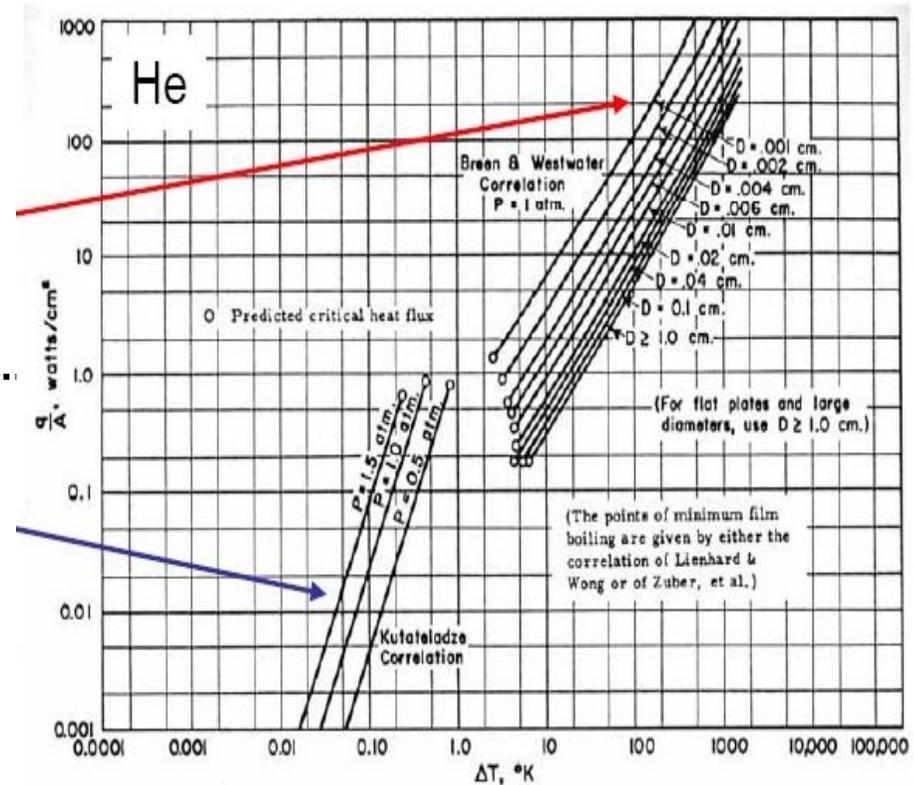
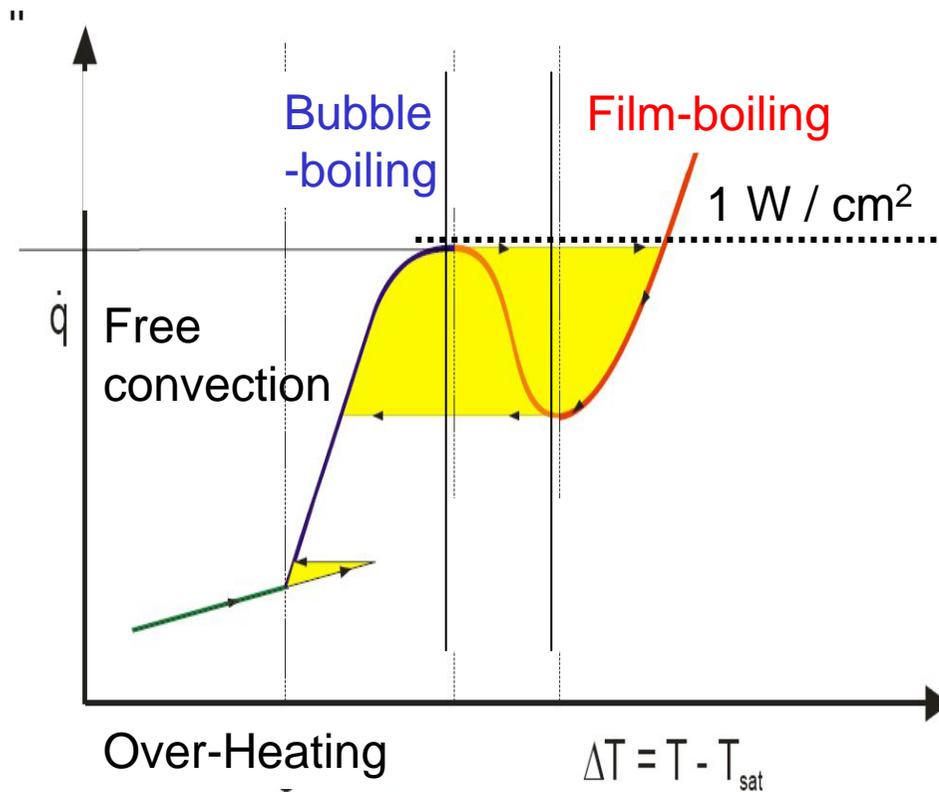
(pressure stability required for TESLA cavities)



Heat Transfer to a Bath of Helium I

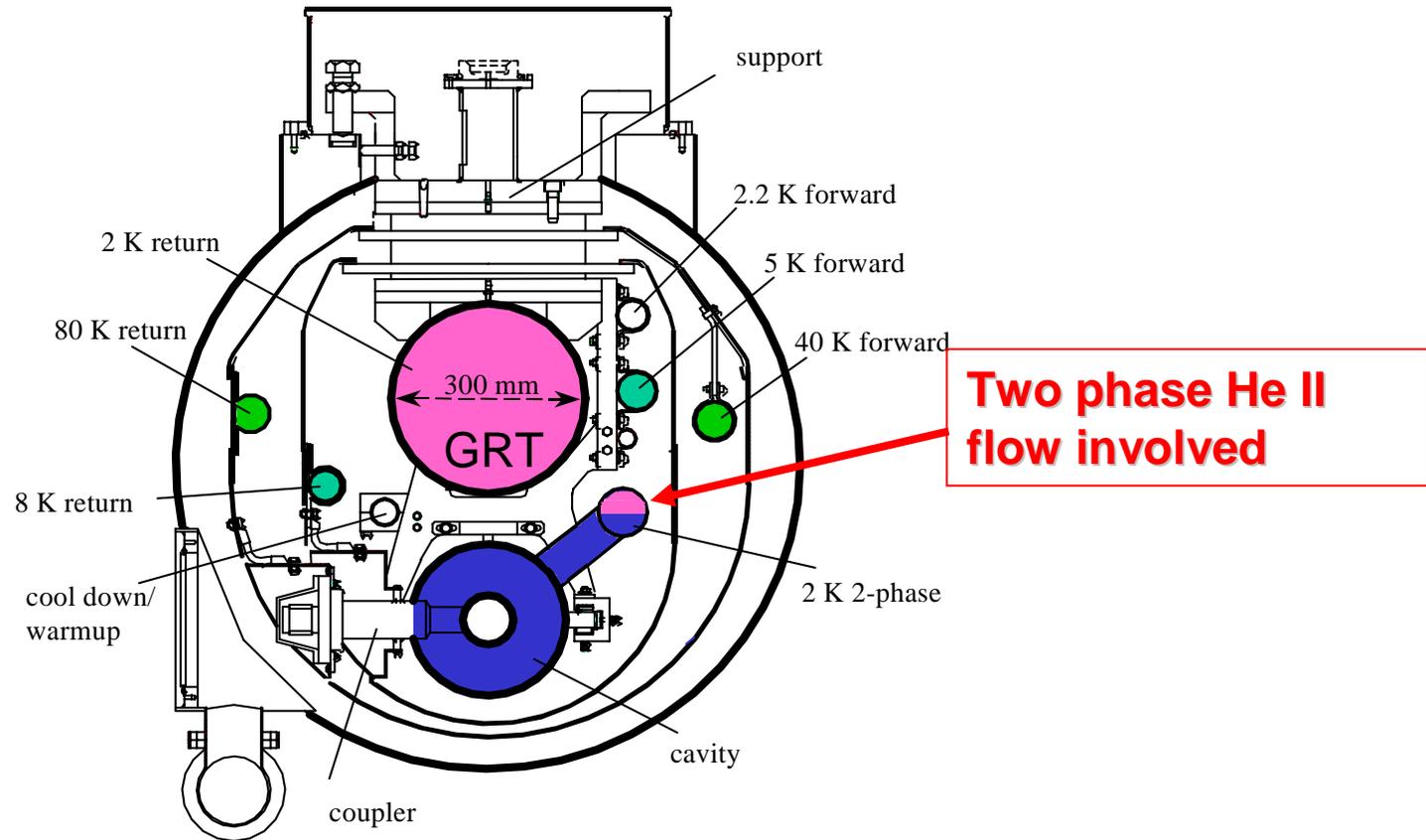
Remember: Helium II bath 1 W/cm²
maximum heat flow density

INSIDE the bath !



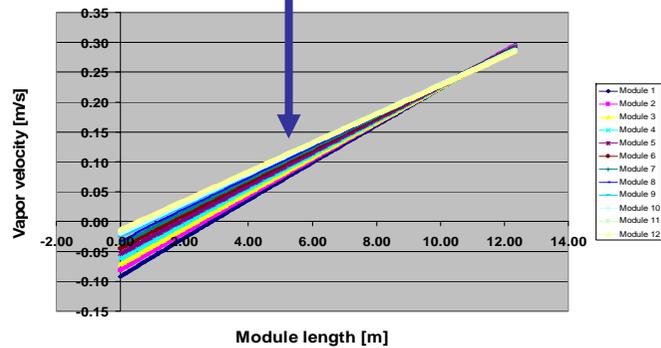
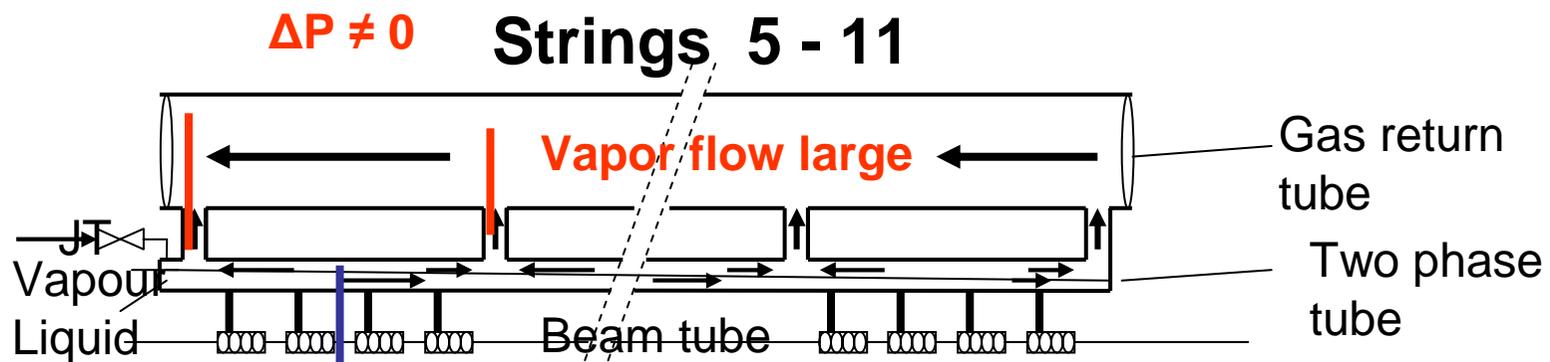
Layout of XFEL-linac cryogenic: Helium II bath cooling

About 1000 1.3 GHz sc cavities will be cooled in a 2K Helium II bath



Disadvantage: Complex 2-phase flow conditions

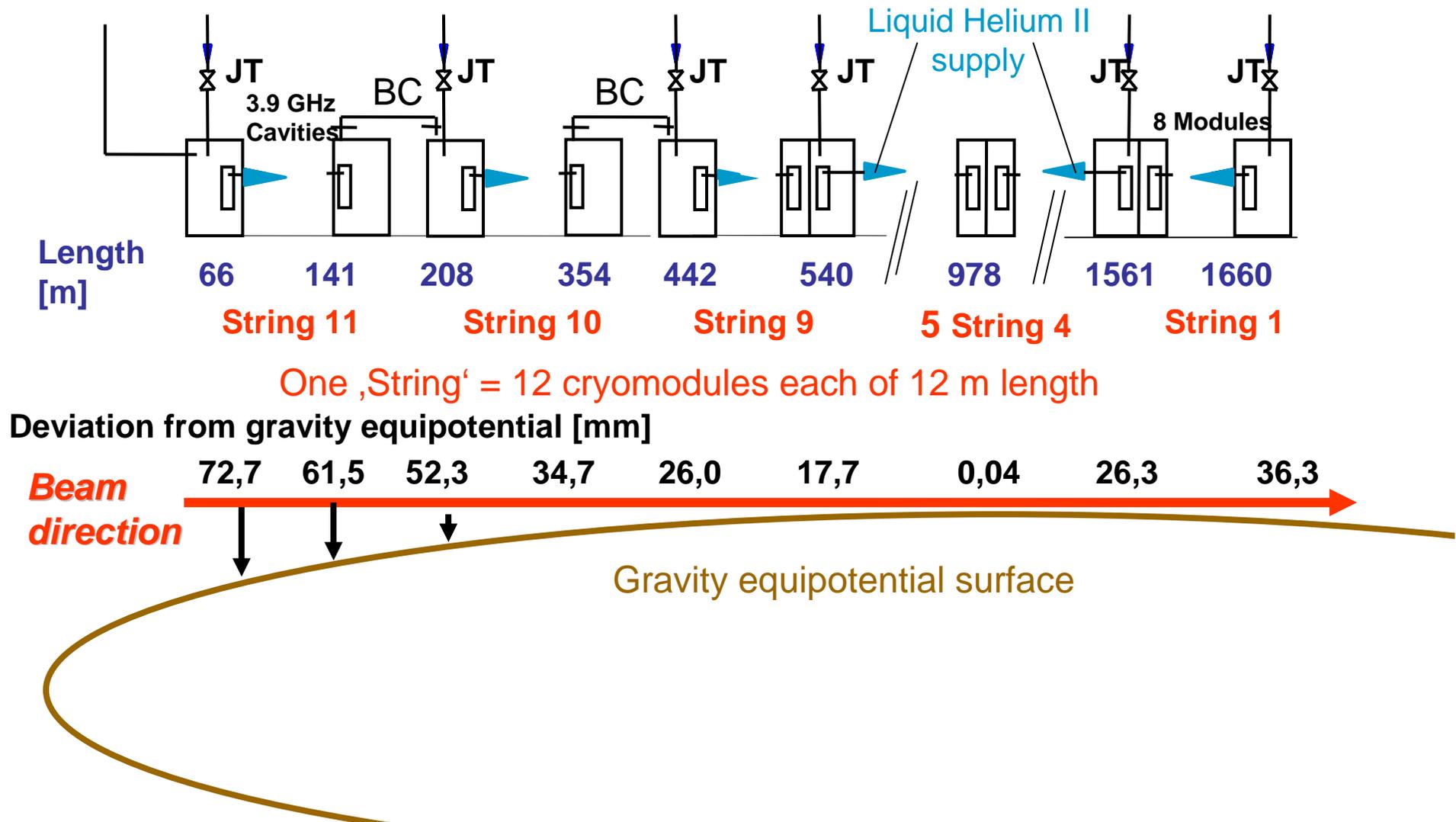
Example: Situation at the start of the XFEL-linac
(refrigerator side)



Vapor flow velocity in 2-phase tube
String 10

Disadvantage: 2-phase flow affected by gravitational forces

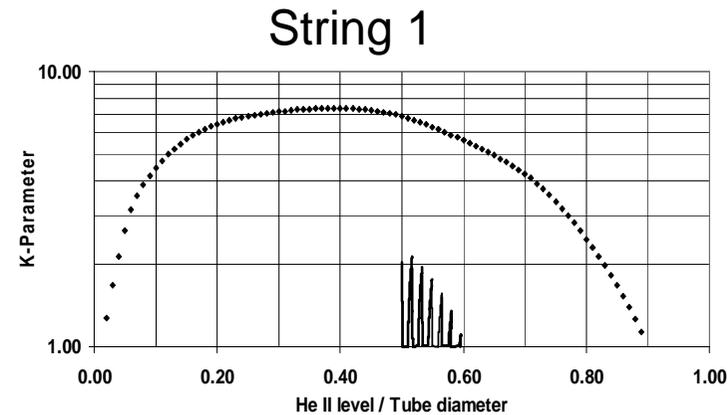
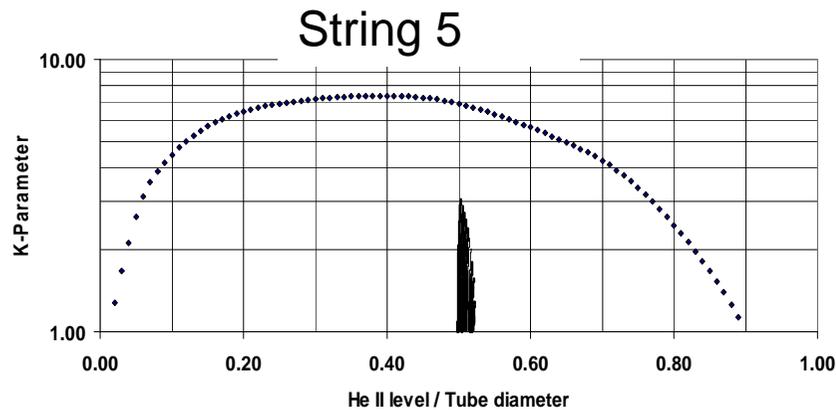
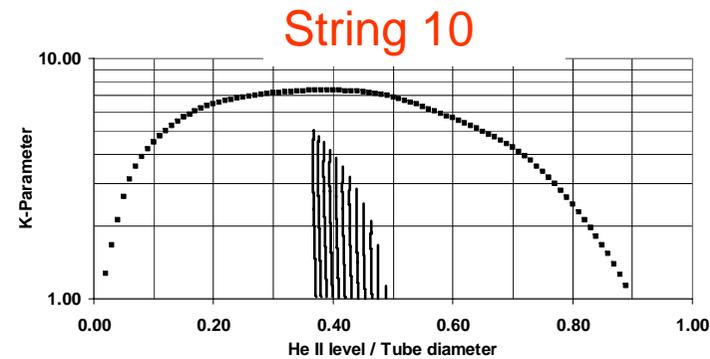
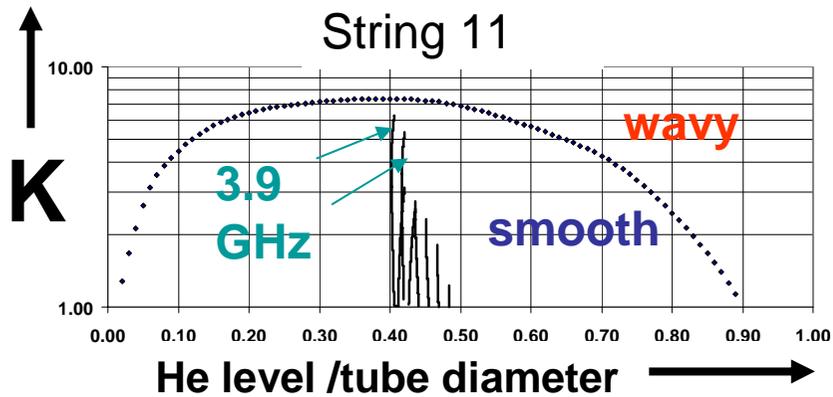
Laser-straight XFEL-linac



Two phase Helium II flow: for the XFEL-linac we want stratified-smooth flow

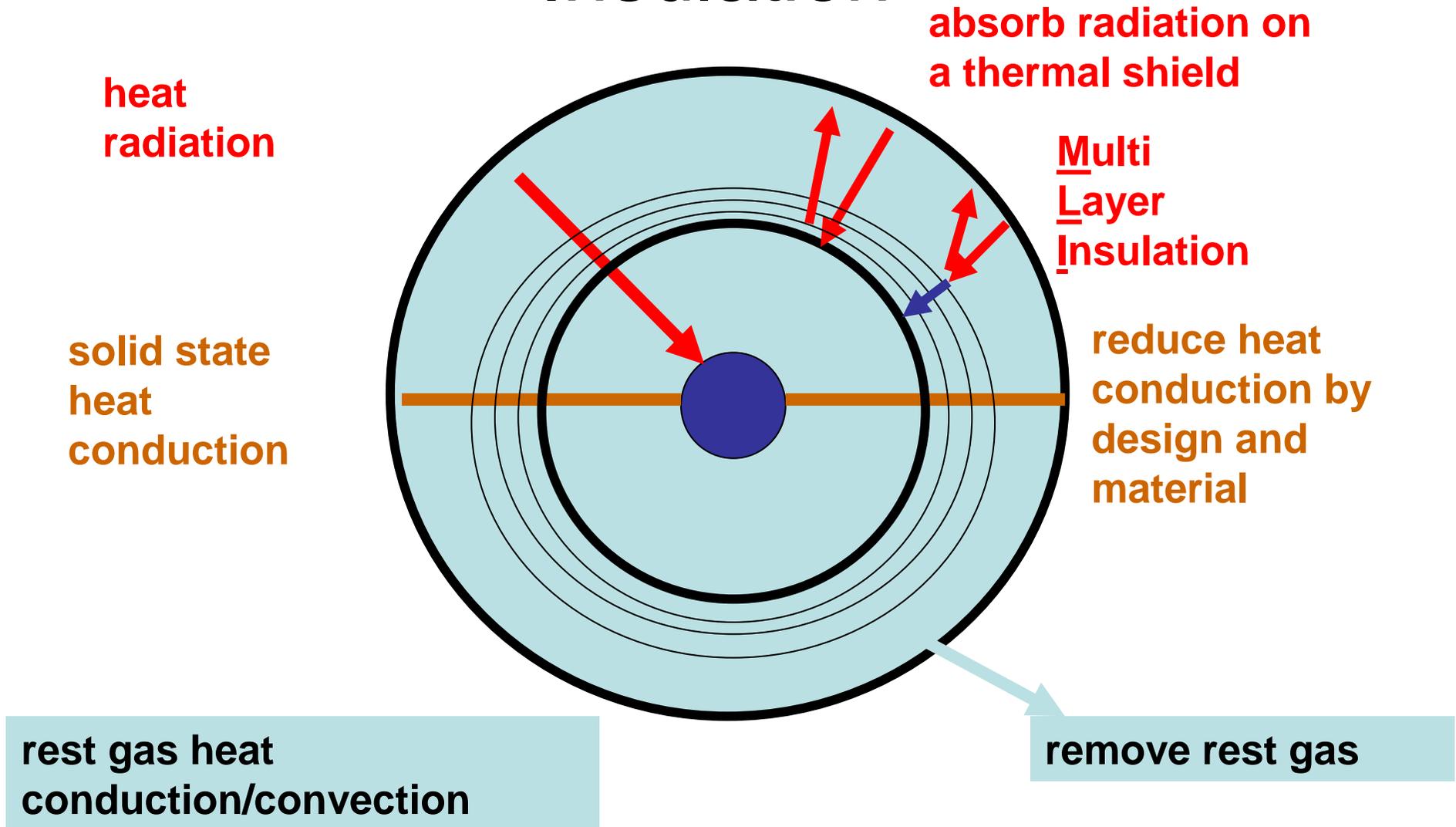
Design operation of XFEL: 2 K, 20 GeV, 23.6 MV/m 15 W/cryomodule

$$K = [(\rho_l * \rho_g * VGS2 * VLS) / ((\rho_l - \rho_g) * g * \mu * \cos(\beta))]^{1/2}$$



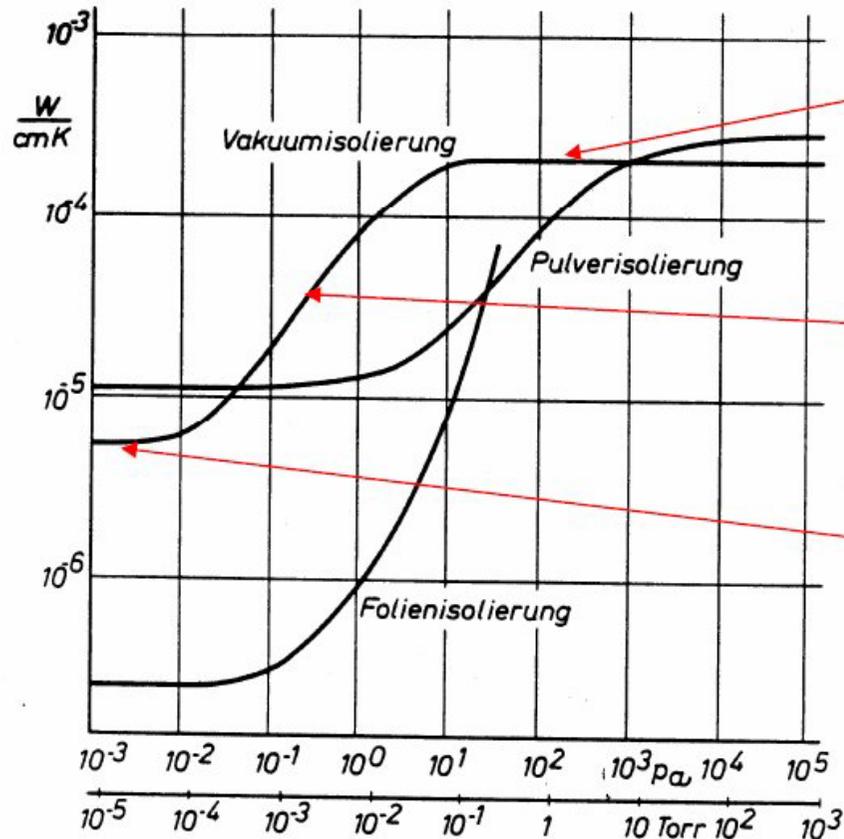
2-ph-flow conditions for cryomodules in different sections of the XFEL-linac

Some Fundamentals of Thermal Insulation



Some Fundamentals of Thermal Insulation: vacuum

heat
conductivity



1. $\Lambda/s \ll 1$: viscous

2. $\Lambda/s \approx 1$: Knudsen

3. $\Lambda/s \gg 1$: molecular

Λ = mean free path of gas molecules

S = cryostat dimension

Some Fundamentals of Thermal Insulation: MLI

Multi Layer Insulation = , Superinsulation'

to limit heat conduction between the MLI-layers:

avoid direct contact of layers, make vacuum pumping possible

MLI-materials:

Aluminum foil

Plastic foil : Mylar Al – coated (one or both sides)

vacuum pumping may be enhanced by small holes in foil

space between foils required to limit heat conduction:

use of ,wrinkled' foils or spacer layers

spacer materials: glas-paper, glas fiber net, paper,.....

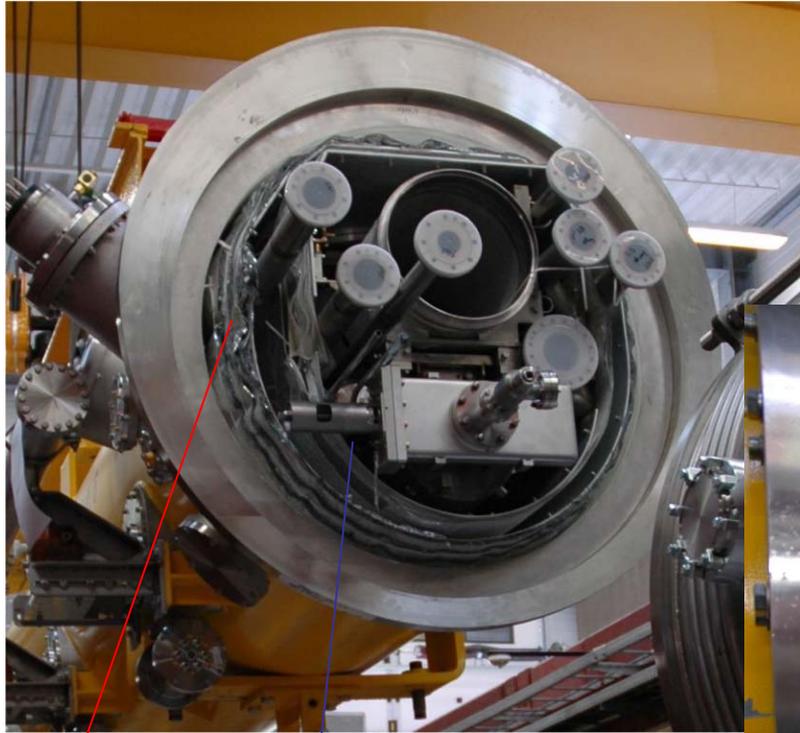
Some Fundamentals of Thermal Insulation: MLI impressions



spacer
glas fiber
net
(vitrolan)



Some Fundamentals of Thermal Insulation: TESLA Cryomodule MLI impressions

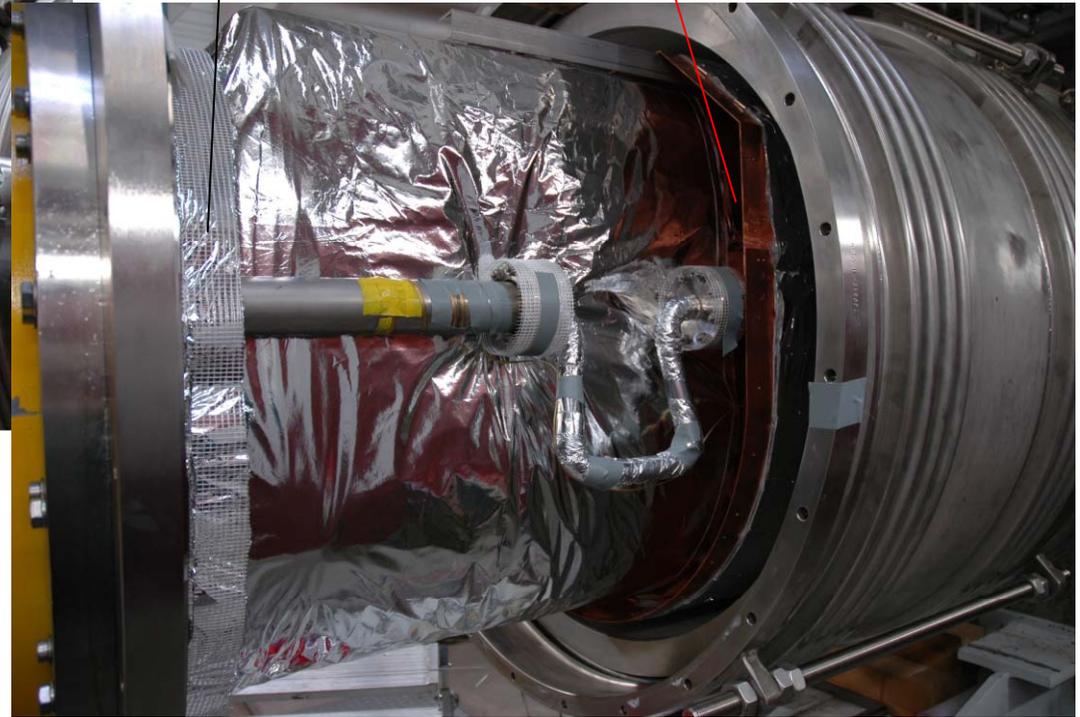


80K
shield

8K
shield

spacer
net

MLI covered Cu
shield of end-cap

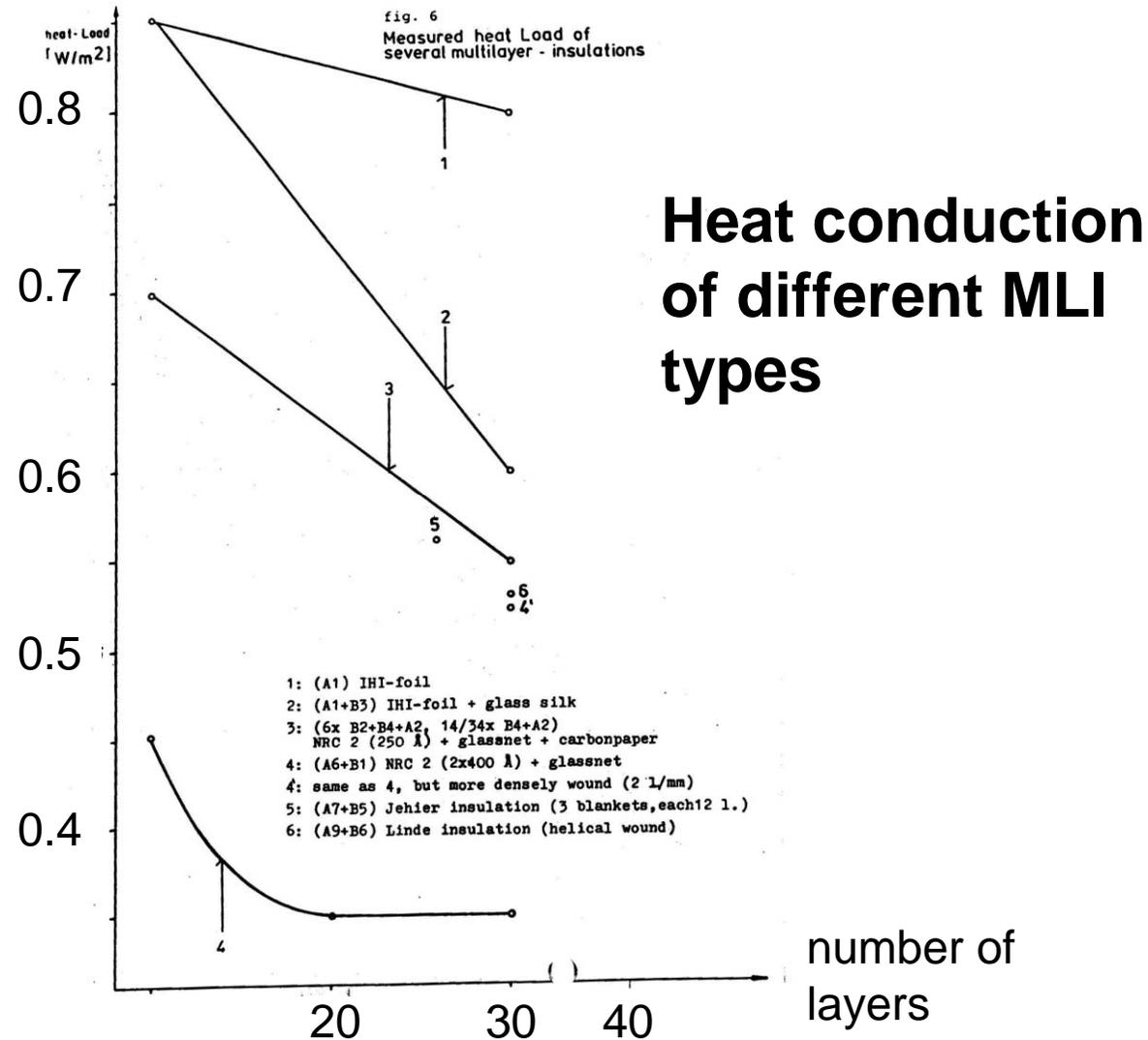


Module connection to end-cap

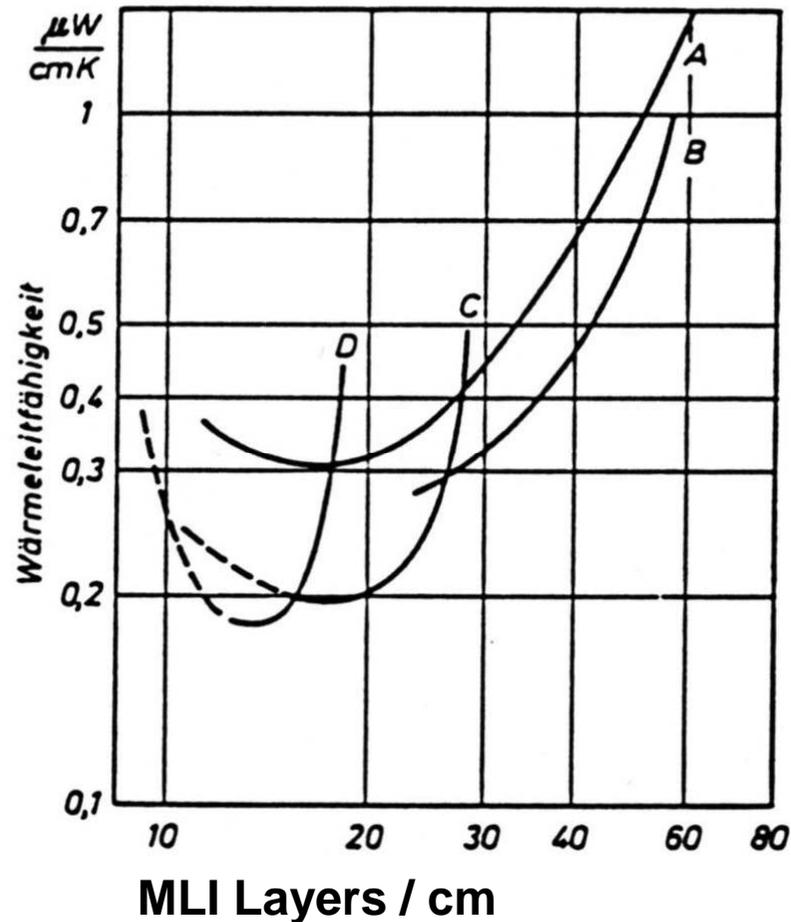
Some Fundamentals of Thermal Insulation: MLI

heat
conduction
W/m²

**For
design:
1 W/m²**



Some Fundamentals of Thermal Insulation: MLI



Heat conductivity of different MLIs vs.

Density of layers

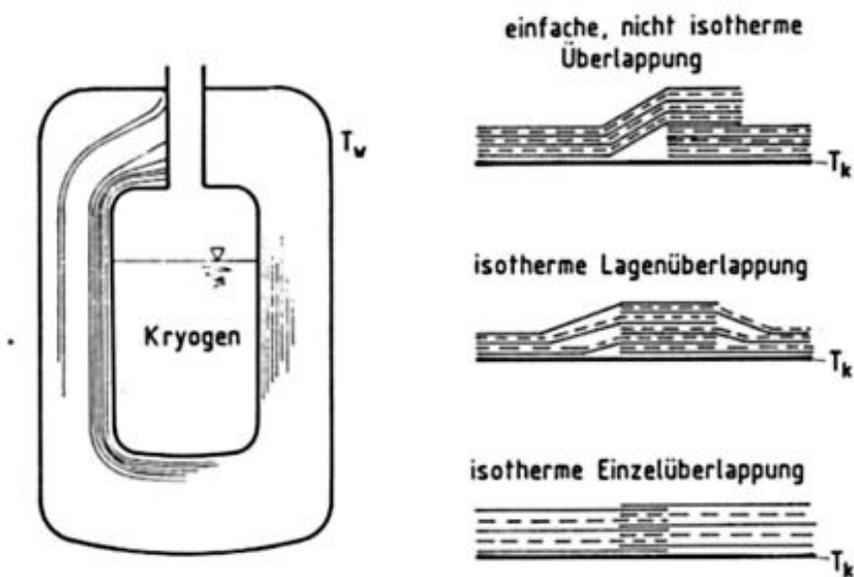
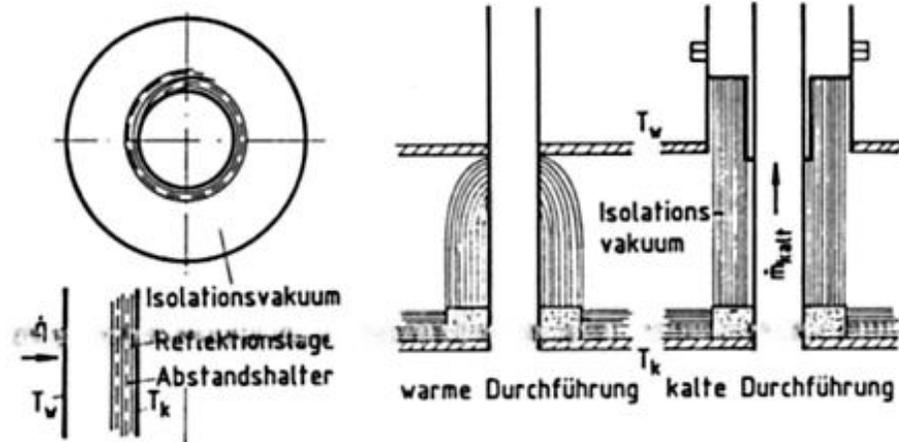
A: AL coated plastic foil

B: AL glas-fiber spacer

C: AL glas-fiber spacer tissue

D: AL glas-fiber paper spacer

Some Fundamentals of Thermal Insulation: MLI



Some Fundamentals of Thermal Insulation: MLI

(see safety section)



2 K Helium Vessel of TESLA Cavity

Note:

All helium process areas inside the cryostat should be covered with about 5-10 layers of MLI to limit the impact of insulation vacuum loss !

Heat input caused by the break down of Insulation vacuum:

40kW / m² without MLI

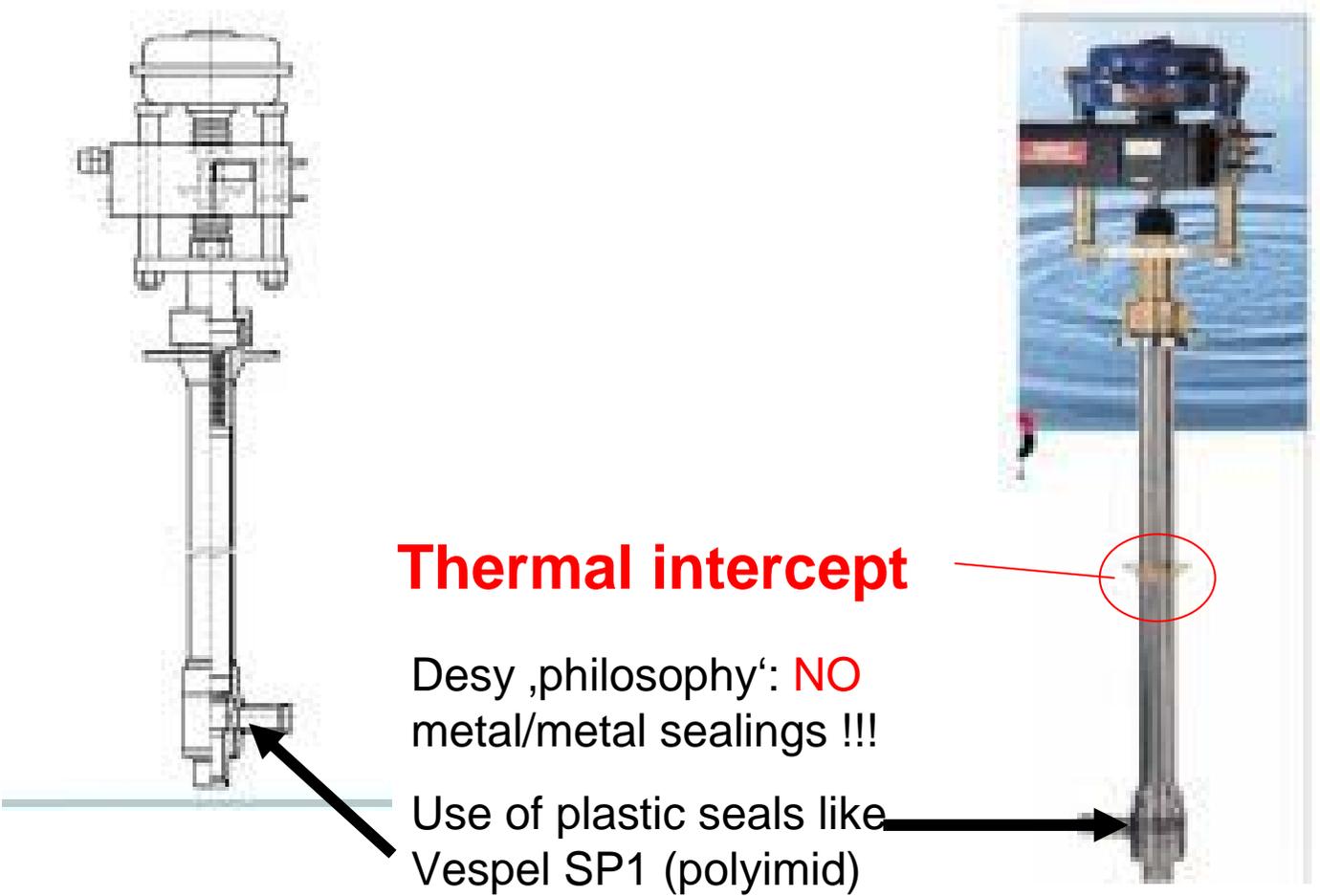
6kW/ m² with MLI

... in addition the Helium vessel get their magnetic shielding



Single parts of magnetic shield and assembly of magnetic shielding

Some Fundamentals of Thermal Insulation: cryogenic valves



Thermal intercept

Desy ,philosophy': **NO**
metal/metal sealings !!!

Use of plastic seals like
Vespel SP1 (polyimid)



Specification: **Valve Sizing Formulas (k_v -Value)**

The calculation for the k_v -value is standardized in DIN/IEC534. For a provisional, simplified sizing for control valves the following basic formulas are usable.

p1	upstream pressure, in bara	ρ	specific gravity, in general and for liquids, in kg/m ³
p2	downstream pressure, in bara	ρ_G	specific gravity of gases at 273K and 1013mbar, in kg/m ³
Δp	pressure drop, in bar	Q_G	volumetric flow for gases at 273K and 1013mbar in m ³ / h
Q	flow of liquids, in m ³ /h	T_1	temperature in K, upstream
W	flow in kg/h	v_1	specific volume of vapor at p_1 and T_1 , in m ³ /kg
		v_2	specific volume of steam/vapour at p_2 and T_2 , in m ³ /kg
		v^*	specific volume of steam/vapour at $p_1/2$ and T_1 , in m ³ /kg

Liquid Service:

m ³ / h	kg / h
$k_v = Q \sqrt{\frac{\rho}{1000 \cdot \Delta p}}$	$k_v = \frac{W}{\sqrt{1000 \cdot \rho \cdot \Delta p}}$

Gas Service:

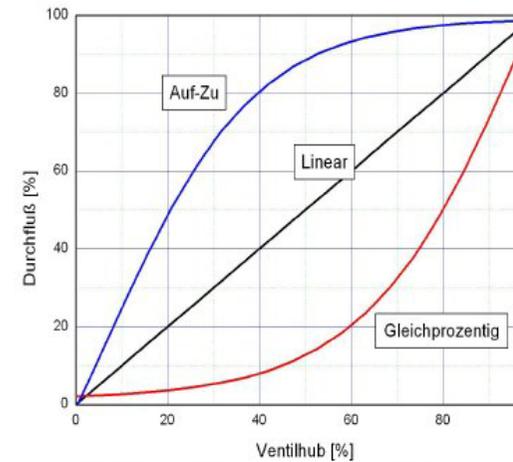
subcritical flow i.e. $p_2 > p_1/2$ and $\Delta p < p_1/2$	
m ³ / h	kg / h
$k_v = \frac{Q_G}{519} \sqrt{\frac{\rho_G \cdot T_1}{\Delta p \cdot p_2}}$	$k_v = \frac{W}{519} \sqrt{\frac{T_1}{\rho_G \cdot \Delta p \cdot p_2}}$

critical flow i.e. $p_2 < p_1/2$ and $\Delta p > p_1/2$	
m ³ / h	kg / h
$k_v = \frac{Q_G}{259.5 \cdot p_1} \sqrt{\rho_G \cdot T_1}$	$k_v = \frac{W}{259.5 \cdot p_1} \sqrt{\frac{T_1}{\rho_G}}$

Vapour / Steam Service:

subcritical flow i.e. $p_2 > p_1/2$ and $\Delta p < p_1/2$	critical flow i.e. $p_2 < p_1/2$ and $\Delta p > p_1/2$
kg / h	kg / h
$k_v = \frac{W}{\sqrt{1000}} \sqrt{\frac{v_2}{\Delta p}}$	$k_v = \frac{W}{\sqrt{1000}} \sqrt{\frac{2 \cdot v^*}{p_1}}$

Definition of K_v -value:
volume flow of water
[m³/h] at $\Delta P = 1$ bar
and T 278 K -313 K
($C_v = 1,17 K_v$ USA)



First part: tutorial objectives

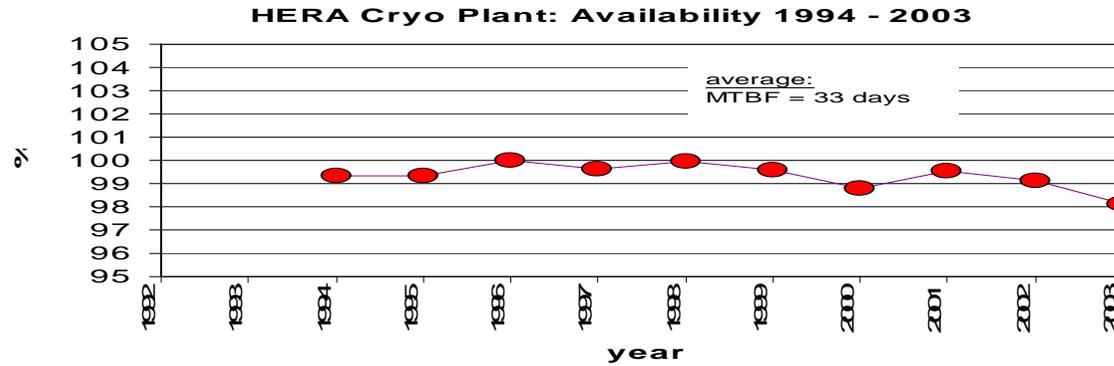
after this part, we should remember:

- The meaning of ,***cryogenic***'
- Carnot refrigerator efficiency
- ,***COP***' of a refrigerator
- Some Helium refrigerator cycles
- Some ,quantum properties' of matter at low temperatures
- Some useful Helium II properties
- Some typical cooling cycles
- Some fundamentals of thermal insulation

Second part: tutorial objectives

after this part, we should remember:

- Measures to increase refrigerator availability
- Helium management considerations
- Suited materials for cryogenic temperatures
- Cryogenic safety aspects
- Basic cryomodule design considerations
- Pressure vessel regulations
- Quality control measures
- Example: TESLA style cryomodule design

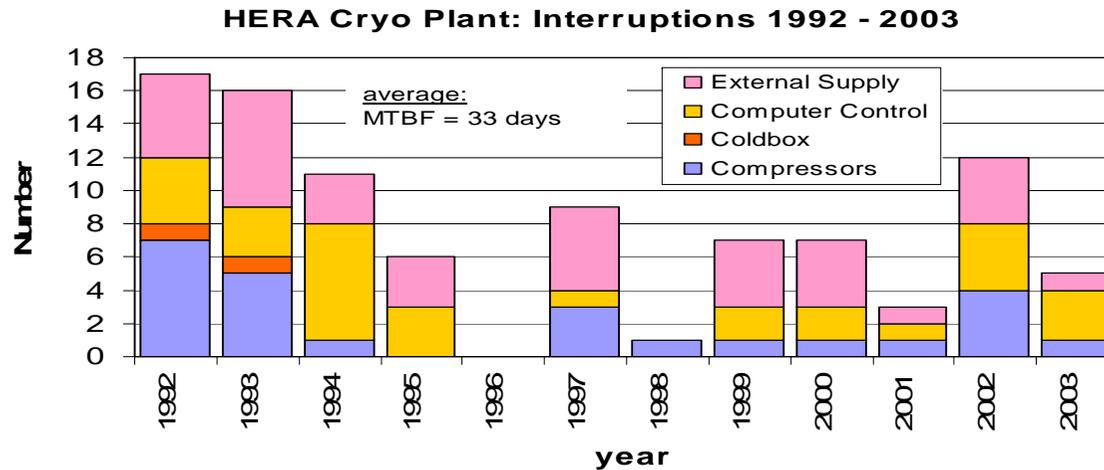


Availability

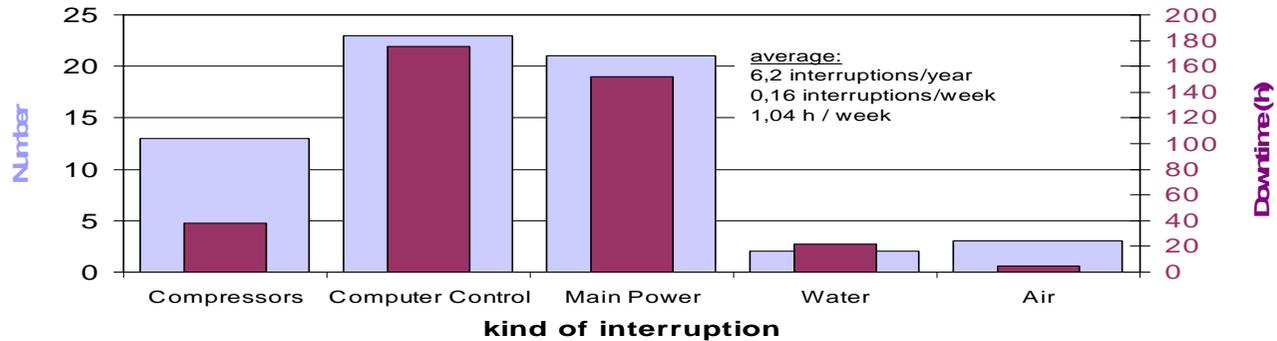
99.6 %

(utilities

excluded)



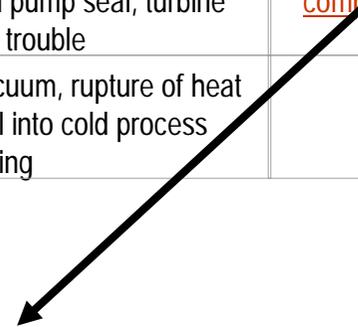
HERA Cryo Plant: Interruptions over 10 years of operation 1994 - 2003



Is there an availability increase by the installation of a complete redundant refrigerator ?

Availability increase by redundant refrigerators?

Rating	Source of unavailability	Example	<u>Multiple</u> refrigerators ... ?
1	External utility failures	Electrical power, cooling water, instrument air failure	would bring no advantage
2	Blockage by frozen out gaseous impurities	Air and/or water vapor	provide somewhat larger tolerance
3	Operational problems	Controls, instrumentation, operators	would be detrimental, because of higher complexity of the system
4	Single component failure not leading to total plant shutdown	Electrical motor burnout, compressor bearings, leaking oil pump seal, turbine bearing trouble	would bring no advantage over <u>component redundancy</u> within a single refrigerator
5	Catastrophic component failure leading to plant shutdown	Loss of insulation vacuum, rupture of heat exchanger, oil spill into cold process piping	would have a positive effect



Redundant compressors and low temperature adsorbers
Easy exchange of turbines and cold compressors

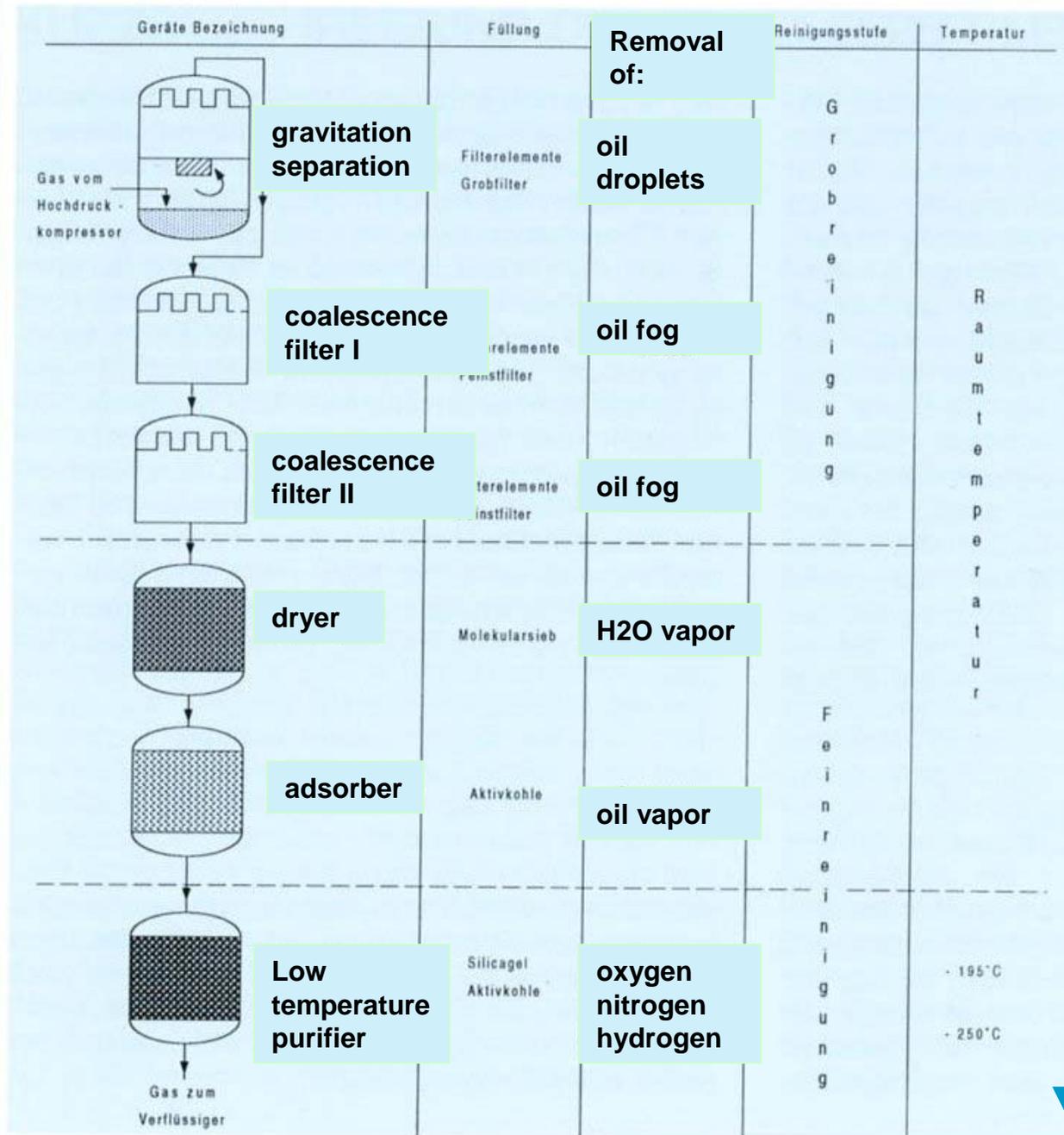
Helium Process Gas Management



Helium gas storage tanks

Liquid Helium storage dewar

Helium process gas purification



HD Coalescence Filter



Helium Dryer



Adsorber



Suited materials for low temperatures



Low temperature embrittlement

Causes overloaded components to fracture spontaneously rather than accommodating the stress by plastic deformation

Appropriate steels for low temperature use are listed in the [Technical Rules for Pressure Vessels AD-Merkblatt W10 /European harmonized technical rules /ASME-code \(USA\)](#) . (In general, materials with face-centered cubic (fcc) crystal structure as copper, nickel, certain copper nickel alloys, zircon and titanium are suitable for cryogenic applications.)

.

European Harmonized Rules

Stainless steels for the use at low temperatures

DIN EN 13445-2

B.2.2.4 Lowest material temperature for austenitic stainless steels Apply also for 2K !

(material spec corresponding to ASTM type AISI may differ !)

Material spec	DIN EN number	ASTM type AISI	T _M (in ° C)
X1NiCrMoCu 31-27-4	1.4563		-270
X1CrNiMoN 25-22-2	1.4466		
X1CrNi 25-21	1.4335	310 L	
X2CrNiMoN 17-13-3	1.4429	316 LN	
X2CrNiMoN 17-11-2	1.4406		
X2CrNiMoN 18-12-4	1.4434		
X2CrNiMo 18-15-4	1.4438	317 L	
X2CrNiN 18-10	1.4311	304 LN	
X2CrNiMo 18-14-3	1.4435	316 L	
X2CrNi 19-11	1.4306	304 L	

Cryogenic safety aspects:

Preventive Measures

Against Pressure Build-up

Redundancy

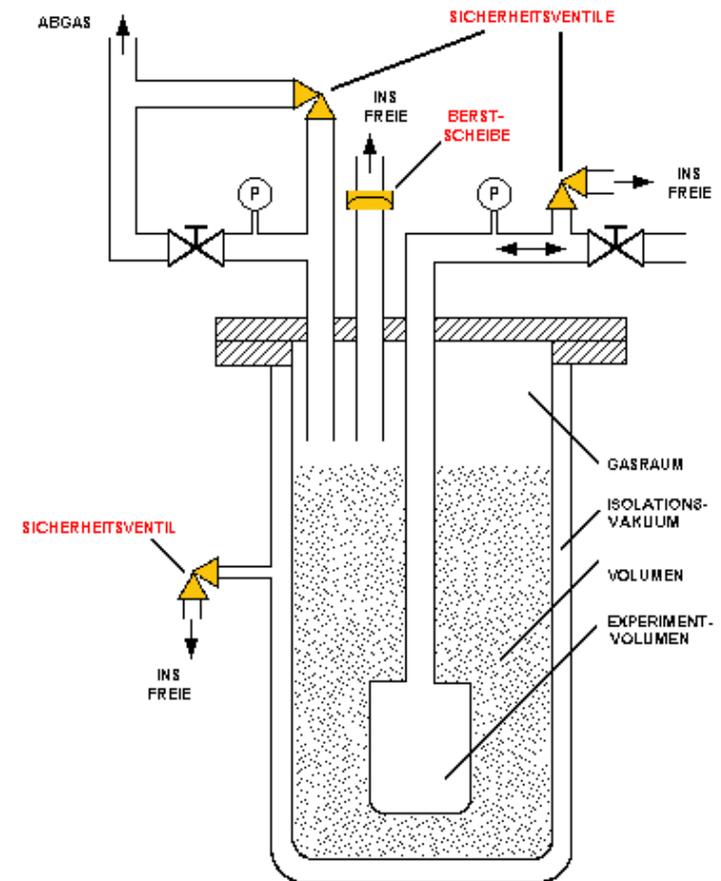
i.e. more safety devices than
required

double safety devices

and

Diversity

i.e. safety devices based on different
mechanisms



Cryogenic safety aspects

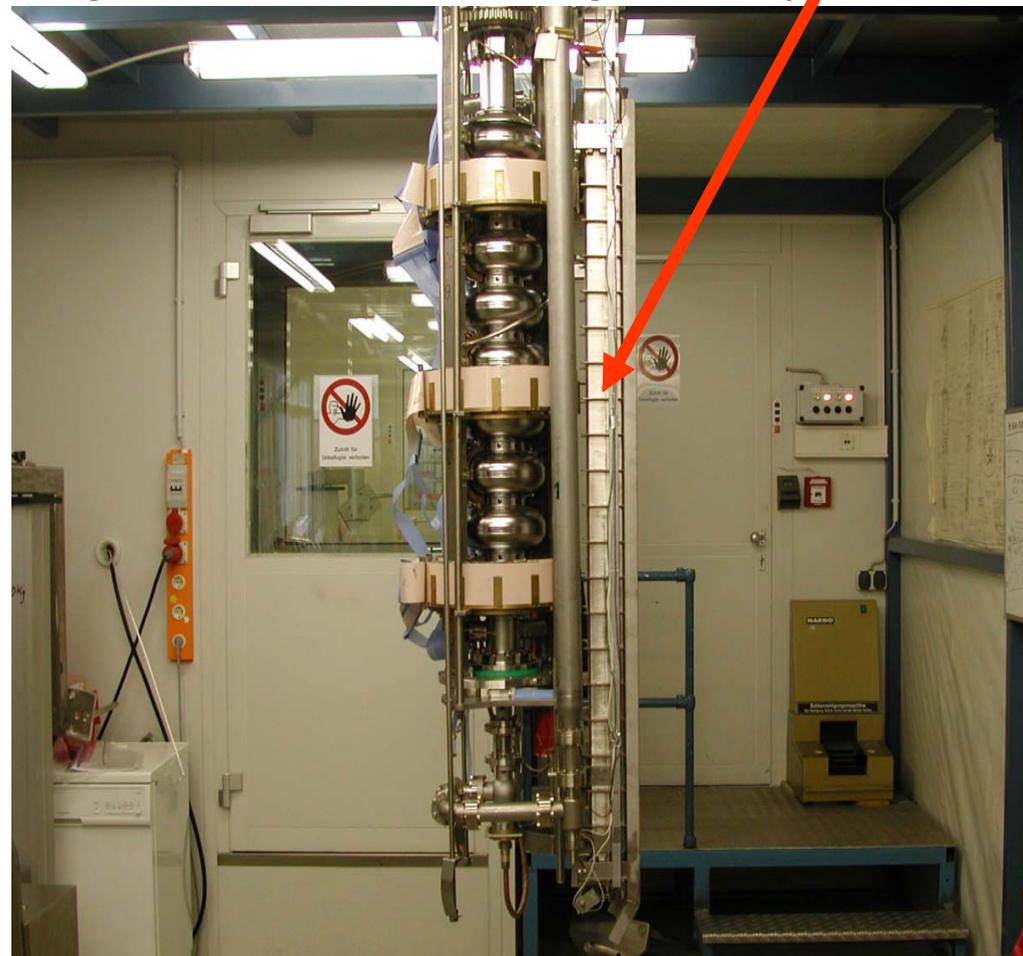
Pressure Build-up by Evaporation

Large air leak into the wave guide of an insert

-> Evaporation of about 2.6 kg/s mass flow through safety valve

**Heat input caused by
the break down of
Insulation vacuum:**

**40kW / m² without MLI
6kW/ m² with MLI**

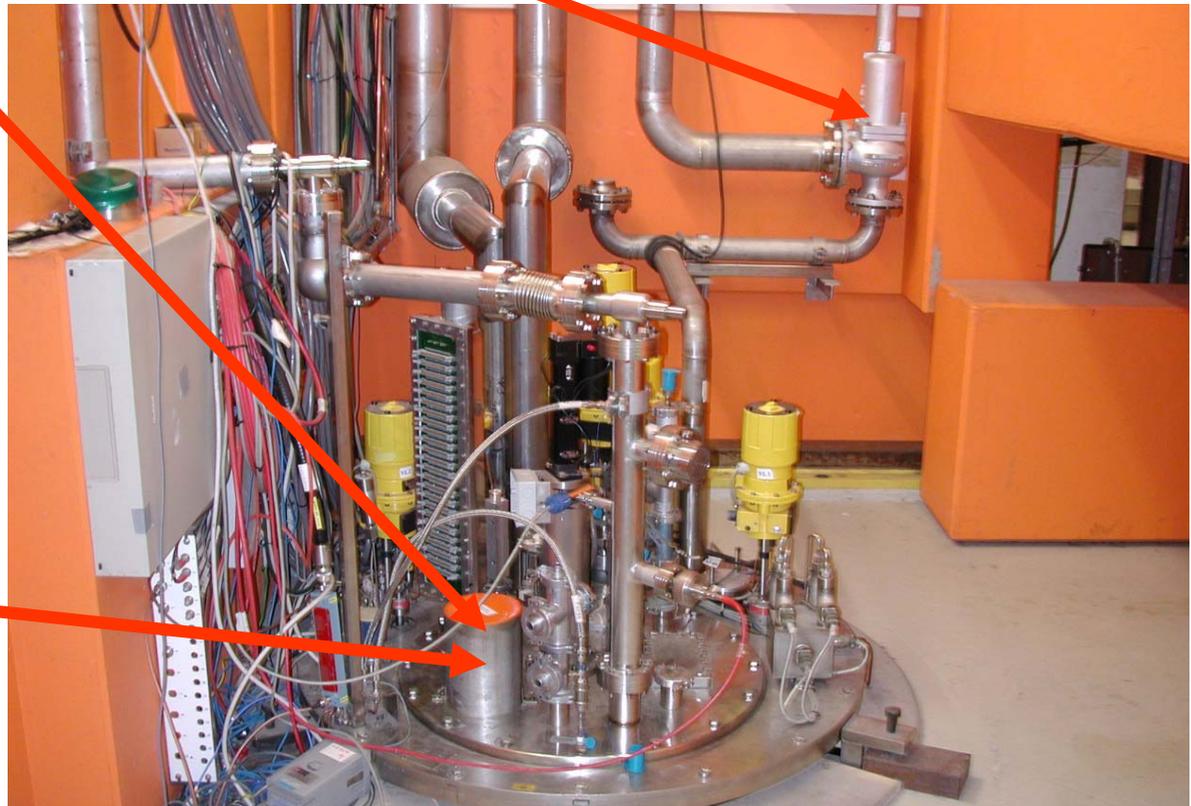


Cryogenic safety aspects

Preventive Measures against Pressure Build-up

Release Flap + Safety Valve

Cautions in the
Vicinity
Of
Release devices !



Safety aspects: Calculation of venting conditions

According to **ASME Code CGA S.1.3-1995**

$$m = \frac{Q}{v * \sqrt{(dh / dv)_P}}$$

$$\frac{\sqrt{v}}{v * \sqrt{(dh / dv)_P}} = f(T)$$

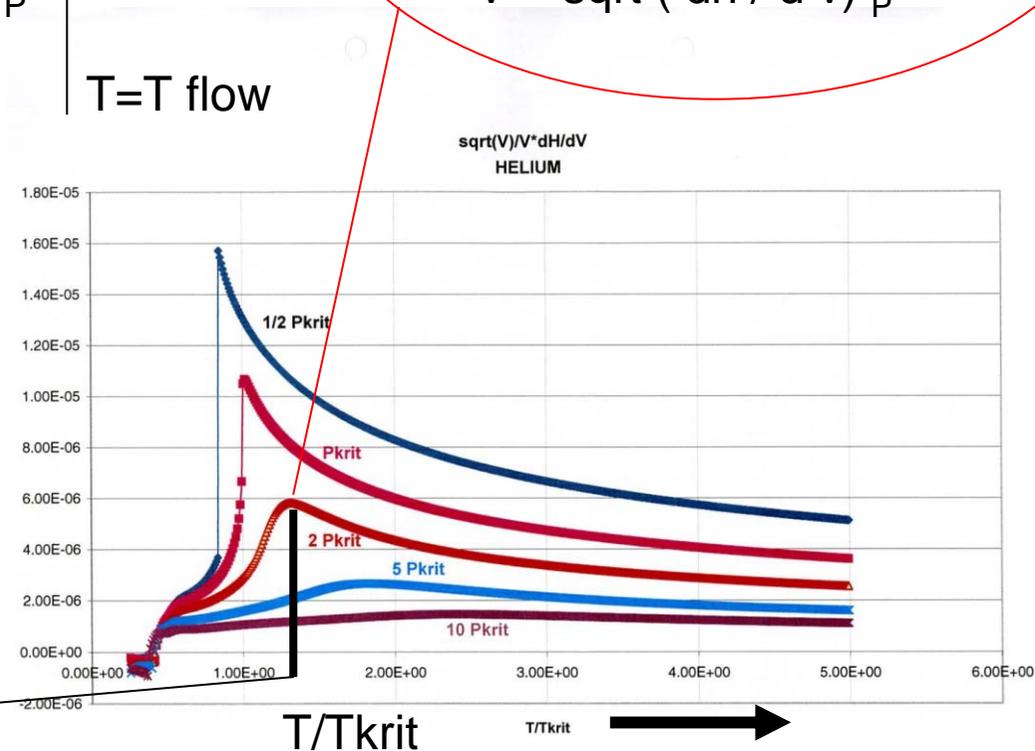
Q – heat input

m – mass flow

V – specific volume

H – specific enthalpy

Maximum at T=T flow



Safety aspects: Spec of safety valves

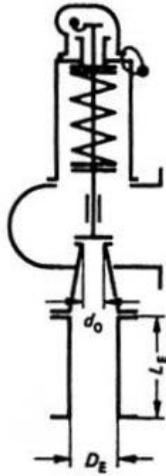


Figure 1

0.4 Gases and vapours

0.4.1 The general relation for the dimensioning of the minimum cross-section of flow is as follows

$$A_0 = \frac{q_m}{\psi \cdot \alpha_w \sqrt{2 \frac{\rho_0}{v}}} \quad (2)$$

where:

A_0 = minimum cross-section of flow in mm²

q_m = mass flow to be discharged in kg/h

ρ_0 = absolute pressure in the pressure chamber in bar

v = specific volume of the medium in the pressure chamber in m³/kg

α_w = the outflow coefficient allotted in the context of component testing

ψ = outflow function

For subcritical pressure ratios $\frac{p_{a0}}{\rho_0} > \left(\frac{2}{k+1}\right)^{\frac{k}{k-1}}$

$$\psi = \sqrt{\frac{k}{k-1}} \cdot \sqrt{\left(\frac{p_{a0}}{\rho_0}\right)^{\frac{2}{k}} - \left(\frac{p_{a0}}{\rho_0}\right)^{\frac{k+1}{k}}} \quad (3)$$

For supercritical pressure ratios

$$\psi = \psi_{\max} = \sqrt{\frac{k}{k+1}} \cdot \left(\frac{2}{k+1}\right)^{\frac{1}{k-1}} \quad (4)$$

where

p_{a0} = absolute counter pressure in bar

k = isentropic exponent of the medium in the pressure chamber

10.4.2 In the case of industrial gases and vapours, the specific volume is calculated from the general relation

$$v = \frac{R_1 \cdot T \cdot Z}{\rho_0} \quad (5)$$

Source: AD pressure vessel code

Safety aspects: procedure

Method used by DESY MKS:

Calculate heat input Q

Find T flow (by ASME code)

Calculate mass flow at T flow (by ASME code)

Calculate sv dimensions (by AD code)

**Safety
Valve in
action.....**

.....



Basic cryomodule design considerations (1)

Task : design a cryomodule for SRF accelerator operation

- Operation mode : pulsed or cw ???
- Fraction of dynamic and static loads ?
- RF operation frequency -> choice of operation temperature
- $\beta = ???$ -> general cavity and cryostat design
- RF main coupler loads -> thermal intercepts
- HOM loads -> design of couplers and absorbers
- ERL machines -> active cooling of HOM absorbers may be required
- Tuners -> warm or cold (extra feedtroughs required ?)
- Magnetic shielding of cavities
- Focusing sc magnets included ? Current leads design....
- Alignment requirements
- Environment -> expected radiation level, tunnel ?.....
- Single individual cryostat or serial production for large accelerator ?

Basic cryomodule design considerations (2)

Task : design a cryomodule for SRF accelerator operation

Some ,formal' aspects:

- Generate a design concept
- Concept for cooling and heat load estimate
- **Risk analysis** -> choice of technical rules & pressure vessel classification
- **Risk analysis** -> safety concept & equipment
- **Pressure vessel code** -> design & construction rules
- **Pressure vessel code** -> choice and control of materials
- **Pressure vessel code** -> welding procedures & management
- **Pressure vessel code** -> third party inspection & test procedures
- **Quality control plan** (in addition to pressure vessel code)
- Design, construction & prototyping
- Testing, testing,testing.....
- Transfer to industrial construction
- Testing, testing,testing....-> pre-series -> serial production

Basic cryomodule design considerations (3)

Task : design a cryomodule for SRF accelerator operation

Some formal Rules, laws, regulations which have to be obeyed in the EU

INCOMPLETE !

- European Pressure Equipment Directive (Richtlinie 97/23/EG für Druckgeräte)
- Richtlinie über elektrische Betriebsmittel (73/23EWG)
- Geräte- und Produktsicherheitsgesetz (GPSG)
- Betriebssicherheitsverordnung (BetrSichV)
- Qualitätsmanagementsysteme DIN EN ISO 9001, August 1994
- European Harmonized Standards like Europäische Norm EN 13445, etc.

Basic cryomodule design considerations (4)

Task : design a cryomodule for SRF accelerator operation

Some ,technical‘ aspects:

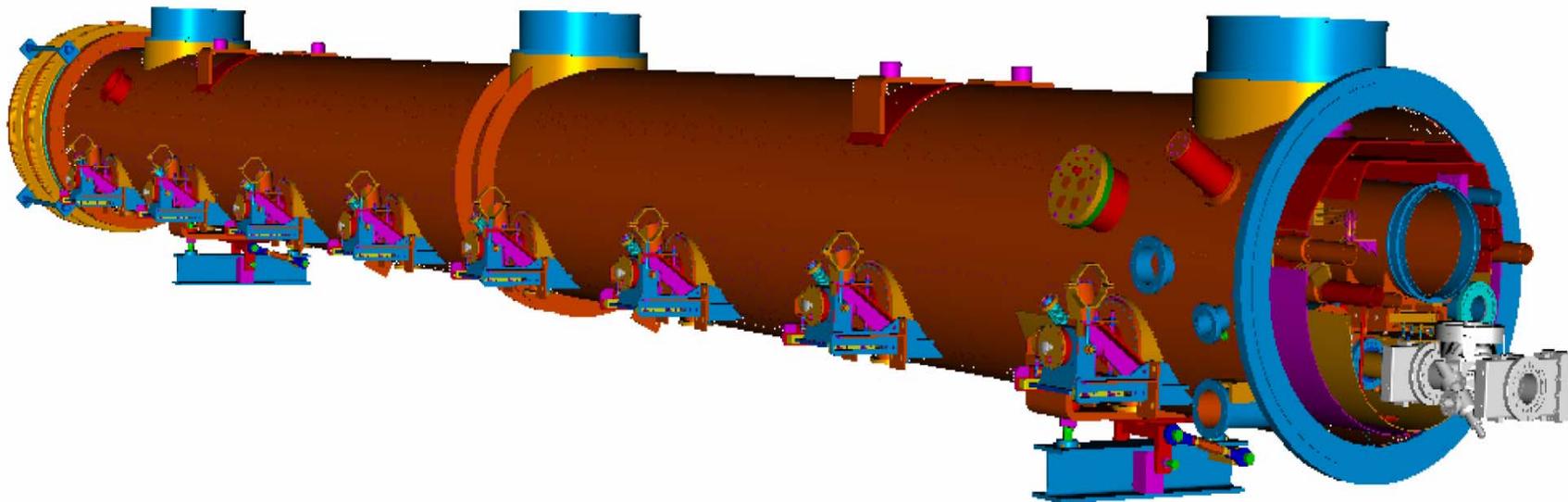
- By the way: the cavities have to work -> **include clean room requirements** from the start for all related components
- Quality insurance procedures: helium leak tests of each and every helium process components required (before, during and after assembly)
- Helium leak testing at a rate of 10^{-8} mbar/l*sec (or better) for the individual componets at ambient temperatures will avoid ,cold-leaks‘ in the order of better than 99%
- DESY ,philosophy‘: **no direct feedthroughs from helium process areas to insulation vacuum for accelerator cryostats !!!!**
- Structural tests (like X-raying of welds) can NOT replace helium leak checks (and vice versa) !!!!
- Welding additives must be qualified for low temperatures -> strict certification of welding procedures & welders; strict quality control organization and management

Example: TESLA-style cryomodule design (INFN Milano/Italy)

Designed for large accelerators -> low costs per length accelerator

-> ,easy' and cheap assembly

-> serves as a ,generic design' for other projects:ERLs,XFEL,ILC.....



Example: TESLA-style cryomodule design

Positions of cavities and Couplers are fixed

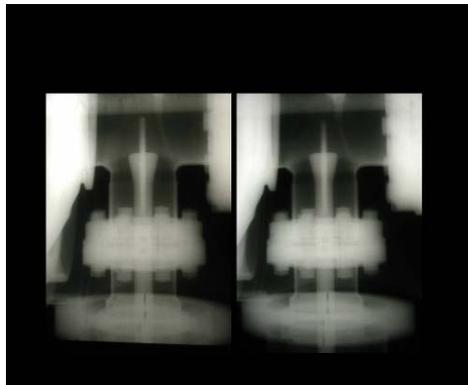
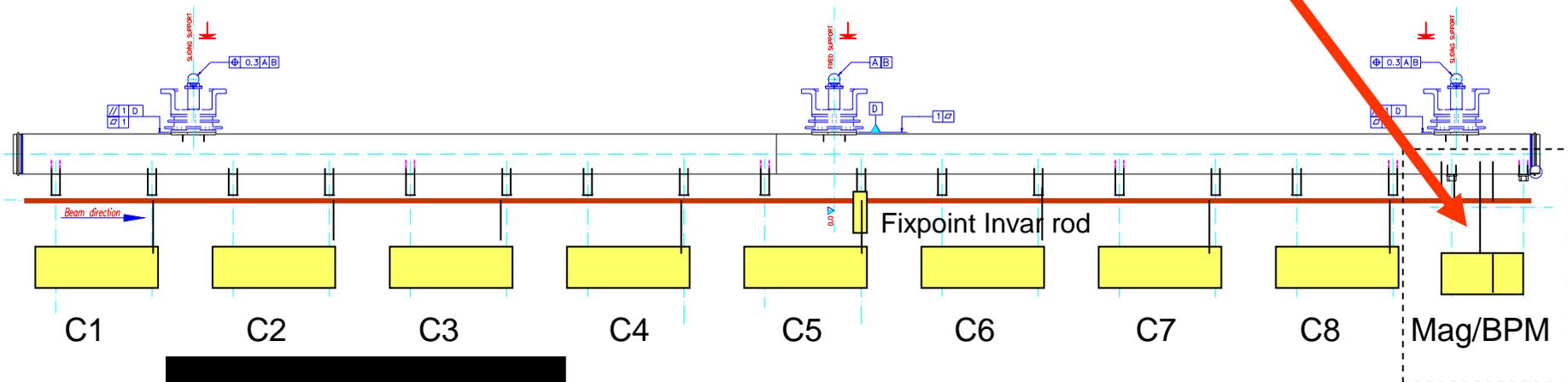
XFEL module type

-->sliding

fixed

Sc magnet package also fixed at invar rod

←sliding



X-ray of coupler position
at 300 K and 2K

TESLA-style module design: 3 design steps

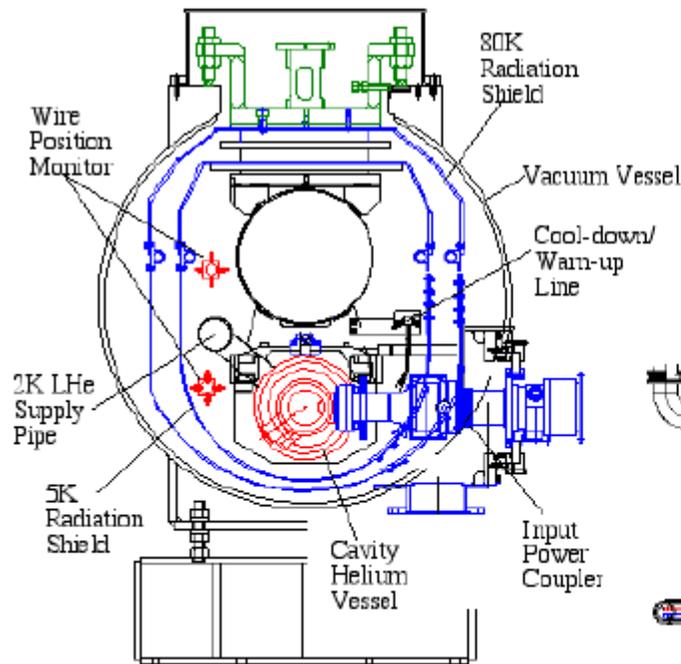
In use for FLASH-linac user facility at DESY

Prototype for XFEL-linac cryomodules (only minor modifications)

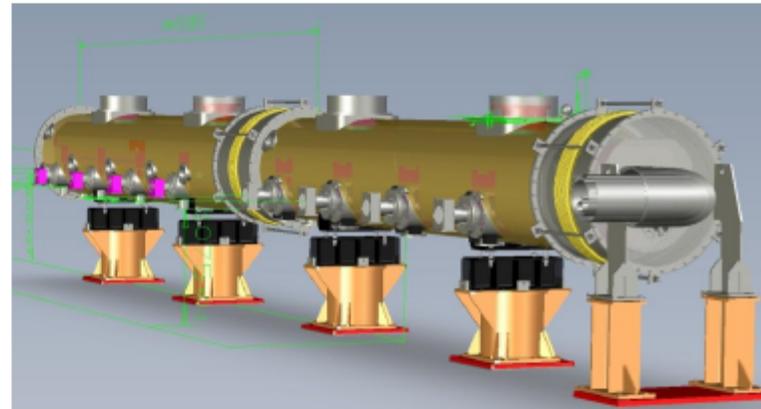


Design of the KEK-STF Cryomodule

- The design of the cross section of the KEK-STF cryomodule is based on the **TTF-III** cryomodule.
- Two cryomodules for the TESLA-like-cavities and the LL-type-cavities are connected with the vacuum bellows, and the total length of the vacuum vessels is 13.25 meter.
- Each cryostat is designed to have four cavities.

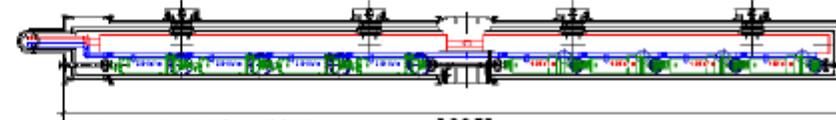


2007/4/23



Cryostat for Tesla-like-cavities

Cryostat for LL-type-cavities



TTC Meeting in FNAL 23-26/April/07

13251

(courtesy of N. Ohuchi et. al KEK)

T4CM Design. The Master Spreadsheet

(courtesy of Don Mitchell and Youri Orlov FNAL)

Microsoft Excel - T4CM_9_MASTER-022807.xls

File Edit View Insert Format Tools Data Window Help

A95 75%

T4CM: Type 4 (9 cavities) Cryomodule Design Master Spreadsheet

updated: 27 Mar 2007

US = Upstream, DS = Downstream

Cryostat DATA		Cavity/Helium Vessel DATA		CAVITY_5 DATA		COLDMASS SUPT DATA		Misc. DATA		Italian date		
	inches	mm		mm		mm		mm				
Vessel Diameter	35	865.20	Cavity length	1247.400		Coldmass Supt hole dia	414	Beamline Vertical Shrinkage	19		(was=15mm)	
Vessel V/L	0.375	9.53	Interconnect below length	71.000	Cavity_5_US Flange "Z"	-632.7	Coldmass location US	4175	MC port hole diam/len	325.0		
US Cav. Flange-to-US Vessel Flange	3.200	233.62	MC center-to-lug dist/len	196.862	Port "A" Z-location	4175	Coldmass location DS	4175	coef. Thermal exp. Stainless steel	0.00001730	mm/m/m/c	0.0000103
US Cav. Flange-to-DS Vessel Flange	7.950	202.17	MC center-to-lug dist/len	946.862	Port "B" Z-location	4175	HGR Centerline	356	coef. Thermal exp. Invar	0.000002	mm/m/m/c	0.00000127
Vessel Flange-to-vessel shell DS	-0.800	-20.50	MC center to DS end flanges	640.800	Port "C" Z-location	4175	ColdMass Support post warm-US	4175	temperature delta	300	deg C	
Vessel Flange-to-vessel shell US	0.610	15.50	Invar mount center to end flanges	150.733	Port "D" Z-location	4175	ColdMass Support post warm-US	4175	HGR pipe "Y" location from vessel centerline	109	mm	
Vessel "Z" length US	222.104	-5658.75	"Z" shrinkage, Invar post-to-Lug	0.253	Port "C" Z-location	21669	ColdMass Support post Warm-DS	4175	MC's Warm "Y" location	19	mm	(was=15mm)
Vessel "Z" length DS	246.853	-6232.37	"Z" shrinkage, Invar post-to-Lug	0.339	Port "D" Z-location	21669	ColdMass Support post Shrink-US	21669	MC's Cold "Y" location	0	mm	
Vessel Length (flange-to-flange)	468.956	11789.50	String length (cav-to-cav flange)	10481.80				MC's Warm "X" location	0	mm		
Vessel shell length US	222.493	-5651.33						MC's Cold "X" location	0.21	mm	(was=0.2mm)	
Vessel shell length DS	239.456	6082.17						Coef. Termal exp. Ti	0.000008	mm/m/m/c	0.0000053	
Cav. String to Vessel CL	9.724	247.00						Coef. Termal exp. Niobium			0.0000049	
VESEL SUPPORT DS	190.945	4850.00										
VESEL SUPPORT US	-171.260	-4350.00										
VESEL PICKUP DS	118.110	3000.00										
VESEL PICKUP US	-118.110	-3000.00										

Main Coupler Location DATA				HGR Support Location DATA				Cavity/Helium Tank Location DATA			
	"Z" Warm	"Z" Cold	"Z" Shrinkage (mm)		"Z" Warm	"Z" Cold	"Z" Shrinkage (mm)		"Z" Warm	"Z" Cold	"Z" Shrinkage (mm)
MC #1 "Z" location	4713.70	4710.77	2.629	Support 1, "Z" location	4821.73	4896.24	25.49	Lug 1, "Z" location	4910.562	4907.407	3.155
MC #2 "Z" location	-3394.50	-3392.66	1.839	Support 2, "Z" location	-5672.67	-5643.29	29.38	Lug 2, "Z" location	-5660.562	-5655.405	5.157
MC #3 "Z" location	-2075.30	-2074.25	1.046	Support 1, "Z" location	-3593.50	-3590.86	2.644	Support 1, "Z" location	-3591.362	-3588.989	2.363
MC #4 "Z" location	-756.10	-755.95	0.255	Support 2, "Z" location	-4350.44	-4327.81	22.63	Support 2, "Z" location	-4341.362	-4336.996	4.366
MC #5 "Z" location	563.10	562.56	0.537	Support 1, "Z" location	-2272.27	-2265.40	6.879	Lug 1, "Z" location	-2272.262	-2270.990	1.272
MC #6 "Z" location	1892.30	1890.97	1.328	Support 2, "Z" location	-3028.22	-3012.53	15.69	Lug 2, "Z" location	-3022.262	-3018.988	3.274
MC #7 "Z" location	3201.50	3199.38	2.120	Support 1, "Z" location	-855.04	-850.10	4.95	Lug 1, "Z" location	-852.962	-852.182	0.780
MC #8 "Z" location	4520.70	4517.79	2.911	Support 2, "Z" location	-1705.99	-1697.16	8.84	Lug 2, "Z" location	-1702.962	-1700.179	2.783
MC #9 "Z" location	5839.90	5836.20	3.703	Support 1, "Z" location	367.18	365.28	1.90	Support 1, "Z" location	366.238	366.227	0.011
				Support 2, "Z" location	-393.76	-391.77	1.99	Lug 1, "Z" location	-393.762	-391.771	1.991
				Support 1, "Z" location	1639.41	1630.65	8.75	Support 1, "Z" location	1636.438	1634.835	0.003
				Support 2, "Z" location	938.47	933.61	4.85	Lug 2, "Z" location	935.438	936.638	-1.200
				Support 1, "Z" location	3011.64	2996.04	15.59	Support 1, "Z" location	3004.638	3003.044	1.594
				Support 2, "Z" location	2280.69	2248.93	31.70	Lug 2, "Z" location	2254.638	2255.046	-0.408
				Support 1, "Z" location	4333.87	4311.42	22.44	Support 1, "Z" location	4323.838	4321.452	2.386
				Support 2, "Z" location	3502.92	3564.31	61.39	Lug 2, "Z" location	3573.838	3573.455	0.383
				Support 1, "Z" location	8556.09	8526.81	29.29	Support 1, "Z" location	8543.038	8539.961	3.177
				Support 2, "Z" location	4905.15	4879.75	25.39	Lug 2, "Z" location	4883.038	4881.863	1.175

Support #2 Support #1 Lug #2 Lug #1 Invar-Rod Post

Hyperlinked to a detailed PDF drawing

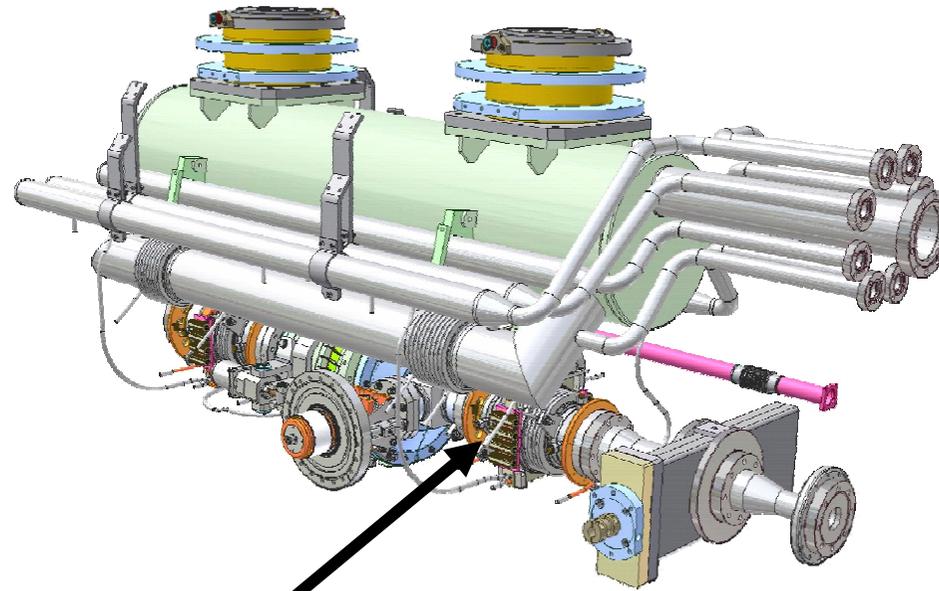
Values which can be modified

Shrinkage Calculations

Cornell University ERL Injector Cryostat

(courtesy of Eric Chojnacki)

Design changes for for
ERL use (cw-operation,
large HOM loads)



HOM absorber

Second part: tutorial objectives

after this part, we should remember:

- Measures to increase refrigerator availability
- Helium management considerations
- Suited materials for cryogenic temperatures
- Cryogenic safety aspects
- Basic cryomodule design considerations
- Pressure vessel regulations
- Quality control measures
- Example: TESLA style cryomodule design

Thank You !